

Analytical and Numerical Study for MHD Radiating Flow over an Infinite Vertical Surface Bounded by a Porous Medium in Presence of Chemical Reaction

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ABSTRACT

The study of non-linear MHD flow with heat and mass transfer characteristics of an incompressible, viscous, electrically conducting and Newtonian fluid over a vertical oscillating porous plate embedded in a porous medium in presence of homogeneous chemical reaction of first order and thermal radiation effects have been analyzed. The fluid considered here is a gray, absorbing/emitting radiation, but a non-scattering medium. At time $t > 0$, the plate temperature and concentration levels near the plate raised linearly with time t . The dimensionless governing coupled, non-linear boundary layer partial differential equations are solved by an efficient, accurate, and extensively validated and unconditionally stable finite difference scheme of the Crank-Nicolson type as well as by the Laplace Transform technique. An increase in porosity parameter (K) is found to depress the fluid velocities and shear stress in the regime. Also it has been found that, when the conduction-radiation (R) increased, the fluid velocities as well as temperature profiles were decreased. It has been found that, when the chemical reaction parameter (C_r) increased, the fluid velocities as well as concentration profiles were decreased. Applications of the study arise in materials processing and solar energy collector systems.

Keywords: Laplace technique, MHD, Absorbing/emitting radiation, Porosity, Chemical reaction.

NOMENCLATURE

A	a constant	\bar{T}_w	fluid temperature at the plate
\bar{a}	absorption coefficient	\bar{T}_∞	fluid temperature in the free stream
C_p	specific heat at constant pressure	t	time parameter
C_r	chemical reaction coefficient	U_0	dimensionless plate velocity
\bar{C}	species concentration	(\bar{u}, \bar{v})	velocity components along (\bar{x}, \bar{y}) -directions
\bar{C}_∞	species concentration in the free stream	β	coefficient of volume expansion for heat transfer
\bar{C}_w	species concentration at the surface	$\bar{\beta}$	coefficient of volume expansion for mass transfer
D	chemical molecular diffusivity	μ	viscosity of fluid
$erfc$	complementary error function	θ	dimensionless fluid temperature
erf	error function	κ	thermal conductivity
Gr_m	mass Grashof number	ν	kinematic viscosity
Gr	thermal Grashof number	ρ	density
g	acceleration due to gravity	σ	electrical conductivity
K_r	porosity of the porous medium	$\bar{\sigma}$	Stefan-Boltzmann constant
M	hartmann number parameter	τ	shearing stress
Nu	Nusselt number	ϕ	dimensionless species concentration
Pr	Prandtl number	Subscripts	
q_r	radiative heat flux	W	conditions on the wall
R_a	thermal radiation	∞	free stream conditions
Sc	Schmidt number		
\bar{T}	temperature		

1. INTRODUCTION

The study of heat and mass transfer with chemical reaction is of great practical importance to engineers and scientists because of its almost universal occurrence in many branches of science and engineering. In particular, the study of chemical reaction, heat and mass transfer with heat radiation is of considerable importance in chemical and hydrometallurgical industries. A reaction is said to be first-order if the rate of reaction is directly proportional to the concentration itself. In many chemical processes, a chemical reaction occurs between a foreign mass and a fluid in which a plate is moving. These processes take place in numerous industrial applications, e.g., polymer production, manufacturing of ceramics or glassware, and food processing Cussler (1998). Chambre and Young (1958) analyzed the diffusion of chemically reactive species in a laminar boundary layer flow. Vajravelu (1986) studied the exact solution for hydrodynamic boundary layer flow and heat transfer over a continuous, moving horizontal flat surface with uniform suction and internal heat generation/absorption. Chamkha (2003) presented an analytical solution for heat and mass transfer by laminar flow of a Newtonian, viscous, electrically conducting fluid and heat generation/absorption.

On the other hand, flow through a porous medium have numerous engineering and geophysical applications, for example, in chemical engineering for filtration and purification process; in agriculture engineering to study the underground water resources; in petroleum technology to study the movement of natural gas, oil and water through the oil reservoirs. In view of these applications, many researchers have studied MHD free convective heat and mass transfer flow in a porous medium; some of them are Raptis and Kafoussias (1982), Sattar (1983) and Kim (2004). Jaiswal and Soundalgekar (2001) obtained an approximate solution to the problem of an unsteady flow past an infinite vertical plate with constant suction and embedded in a porous medium with oscillating plate temperature. The unsteady flow through a highly porous medium in the presence of radiation was studied by Raptis and Perdikis (2004). Sahin (2008) investigated the effect of transverse periodic permeability oscillating with time on the heat transfer flow of a viscous incompressible fluid through a highly porous medium bounded by an infinite vertical porous plate, by means of series solution method. Sahin (2010) studied the effect of transverse periodic permeability oscillating with time on the free convective heat transfer flow of a viscous incompressible fluid through a highly porous medium bounded by an infinite vertical porous plate subjected to a periodic suction velocity.

If the temperature of surrounding fluid is rather high, radiation effects play an important role and this situation does not exist in space technology. In such cases one has to take into account the effect of thermal radiation and mass diffusion. Boundary layer flow on moving horizontal surfaces was studied by Sakiadis (1961). The effects of transversely applied magnetic field on the flow of an electrically conducting fluid past

an impulsively started isothermal vertical plate was studied by Soundalgekar *et al.* (1979). MHD effects on impulsively started vertical infinite plate with variable temperature in the presence of transverse magnetic field were studied by Soundalgekar *et al.* (1981). The dimensionless governing equations were solved using Laplace transform technique. Soundalgekar and Takhar (1993) have considered the radiation free convection flow of an optically thin gray- gas past a semi- infinite vertical plate. Radiation effects on mixed convection along isothermal vertical plate were studied by Hossain and Takhar (1996). In all above studies, the stationary vertical plate is considered. Raptis and Perdikis (1999) studied the effects of thermal radiation and free convection flow past a moving vertical plate. The governing equations were solved analytically. Also, Sahin and Liu (2010) analyzed the effects of mixed convection and mass transfer of three-dimensional oscillatory flow of a viscous incompressible fluid past an infinite vertical porous plate in presence of transverse sinusoidal suction velocity oscillating with time and a constant free stream velocity. Singh (2011) investigated the flow of fluid through porous medium bounded by vertical channel with slip-flow condition and in the presence of thermal radiation and the fluid is of optically thin with relatively low-density. Recently, Sahin (2011) investigated the effects of radiation and chemical reaction on a steady mixed convective heat and mass transfer past an infinite vertical permeable plate with constant suction taking into account the induced magnetic field. A study of unsteady laminar hydro magnetic flow and heat transfer in a porous channel with temperature-dependent properties was presented by Chamkha (2001). Sahin and Kalita (2012) investigated the effects of porosity and magneto hydrodynamic on a horizontal channel flow of a viscous incompressible electrically conducting, Newtonian and radiating fluid through a porous medium in the presence of thermal radiation and transverse magnetic field. Jaiswal and Soundalgekar (2001) obtained an approximate solution to the problem of an unsteady flow past an infinite vertical plate with constant suction and embedded in a porous medium with oscillating plate temperature. Kumar and Verma (2011) studied the problem of an unsteady flow past an infinite vertical permeable plate with constant suction and transverse magnetic field with oscillating plate temperature.

Magneto hydrodynamic mixed free-forced heat and mass convective steady incompressible laminar boundary layer flow of a gray optically thick electrically conducting viscous fluid past a semi-infinite vertical plate for high temperature and concentration differences have studied by Emad and Gamal (2005). Orhan and Kaya (2008) investigated the mixed convection heat transfer about a permeable vertical plate in the presence of magneto and thermal radiation effects using the Keller box scheme, an efficient and accurate finite-difference scheme. Ghosh *et al.* (2009) considered an exact solution for the hydro magnetic natural convection boundary layer flow past an infinite vertical flat plate under the influence of a transverse magnetic field with magnetic induction effects and the transformed ordinary differential equations are solved exactly. On the other hand, Ghosh and Bég (2008) for unsteady convection in porous media, Bég *et al.* (2009)

for coupled species and heat diffusion in nonlinear porous media (using a network electrical simulator), Zueco and Bég (2009) for hydro magnetic gas flow from a two-dimensional wedge in porous media. Muthucumaraswamy and Janakiraman (2006) studied the thermal radiation effects on flow past an impulsively started infinite vertical plate with uniform temperature and variable mass diffusion in the presence of transverse applied magnetic field. The governing equations are solved by the Laplace-transform technique. Rajput and Kumar (2012) considering the radiation effects on MHD flow past an impulsively started vertical plate with variable heat and mass transfer by Laplace transform technique. Ahmed and Kalita (2012) presented the magneto hydrodynamic transient convective radiative heat transfer in an isotropic, homogenous porous regime adjacent to a hot vertical plate using the Laplace transform technique. Such a study has not appeared in the literature and constitutes an important addition to the area of porous media convection studies in presence of transverse magnetic field. Chamkha et al. (2002) considered the natural convection flow from an inclined, semi-infinite, impermeable flat plate embedded in a variable porosity porous medium due to solar radiation and in the presence of an externally applied magnetic field. Chamkha (1997) presented the model for Darcian and non-Darcian effects of the porous medium and the Hall effects of magneto hydrodynamics. It is assumed that the magnetic Reynolds number is small so that the induced magnetic field is neglected. The flow is assumed unsteady, laminar, and incompressible.

In this paper, we consider the effects of chemical reaction as well as magnetic field on the heat and mass transfer of Newtonian fluids over an infinite vertical oscillating plate with variable mass diffusion. The magnetic field is imposed transversely to the plate. The temperature and concentration of the plate is oscillating with time about a constant non-zero mean value. The conservation equations are normalized and then solved using both the Laplace Transform technique and stable finite difference scheme of the Crank-Nicolson type. Excellent agreement is obtained between both analytical and numerical methods.

2. MATHEMATICAL ANALYSIS

Thermal radiation and mass transfer effects on unsteady MHD flow of a viscous incompressible fluid past along a vertical oscillating plate with variable temperature and also with variable mass diffusion in the presence of transverse applied magnetic field and chemical reaction of first order have been studied. The \bar{x} axis is taken along the plate in the vertical upward direction and the \bar{y} axis is taken normal to the plate. Initially it is assumed that the plate and fluid are at the same temperature \bar{T}_∞ in the stationary condition with concentration level \bar{C}_∞ at all the points. At time, $\bar{t} > 0$ the plate is given an oscillatory motion in its own plane with velocity $U_0 \cos(\omega \bar{t})$. At the same time the plate temperature is raised linearly with time \bar{t} and also mass is diffused from the plate linearly with time. A transverse magnetic field of uniform strength B_0 is assumed to be applied normal to the plate. The induced magnetic field and viscous dissipation is assumed to be

negligible as the magnetic Reynolds number of the flow is taken to be very small. The fluid considered here is gray, absorbing/emitting radiation but a non-scattering medium. Then by usual Boussinesq's approximation, the unsteady flow is governed by the following equations.

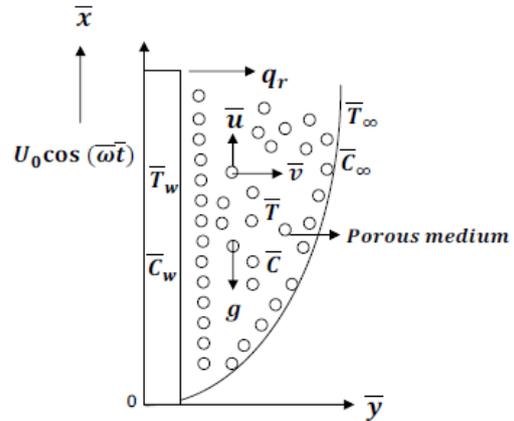


Fig. 1. Physical configuration and coordinate system

$$\frac{\partial \bar{u}}{\partial \bar{t}} = g\beta(\bar{T} - \bar{T}_\infty) + g\bar{\beta}(\bar{C} - \bar{C}_\infty) + \nu \frac{\partial^2 \bar{u}}{\partial \bar{y}^2} - \frac{\sigma B_0^2}{\rho} \bar{u} - \frac{\nu}{K_r} \bar{u} \quad (1)$$

$$\rho C_p \frac{\partial \bar{T}}{\partial \bar{t}} = \kappa \frac{\partial^2 \bar{T}}{\partial \bar{y}^2} - \frac{\partial q_r}{\partial \bar{y}} \quad (2)$$

$$\frac{\partial \bar{C}}{\partial \bar{t}} = D \frac{\partial^2 \bar{C}}{\partial \bar{y}^2} - C_r(\bar{C} - \bar{C}_\infty) \quad (3)$$

The initial and boundary conditions are:

$$\begin{aligned} \bar{t} \leq 0: \bar{u} &= 0, \bar{T} = \bar{T}_\infty, \bar{C} = \bar{C}_\infty \quad \forall y \\ \bar{t} > 0: \bar{u} &= U_0 \cos(\omega \bar{t}), \bar{T} = \bar{T}_\infty + (\bar{T}_w - \bar{T}_\infty) A \bar{t} \\ \bar{C} &= \bar{C}_\infty + (\bar{C}_w - \bar{C}_\infty) A \bar{t} \text{ at } y = 0 \\ \bar{t} > 0: \bar{u} &\rightarrow 0, \bar{T} \rightarrow \bar{T}_\infty, \bar{C} \rightarrow \bar{C}_\infty \text{ as } y \rightarrow \infty \end{aligned} \quad (4)$$

The local radiant absorption for the case of an optically thin gray gas ((2004), (2006), (2012)) is expressed as

$$\frac{\partial q_r}{\partial \bar{y}} = -4\bar{a}\bar{\sigma}(\bar{T}_\infty^4 - \bar{T}^4) \quad (5)$$

Where $\bar{\sigma}$ and \bar{a} are the Stefan-Boltzmann constant and the Mean absorption coefficient, respectively. Following (2004), (2006), (2012) and others, we assume that the temperature differences within the flow are sufficiently small so that \bar{T}^4 can be expressed as a linear function of \bar{T} after using Taylor's series to expand \bar{T}^4 about the free stream temperature \bar{T}_∞ and neglecting higher-order terms. This results in the following approximation:

$$\bar{T}^4 \cong 4\bar{T}_\infty^3 \bar{T} - 3\bar{T}_\infty^4 \quad (6)$$

$$\rho C_P \frac{\partial \bar{T}}{\partial t} = \kappa \frac{\partial^2 \bar{T}}{\partial y^2} - 16\bar{\alpha}\bar{\sigma}\bar{T}_\infty^3(\bar{T} - \bar{T}_\infty) \quad (7)$$

Introducing the following non-dimensional quantities:

$$\begin{aligned} y &= \frac{u_0 \bar{y}}{v}, \quad u = \frac{\bar{u}}{u_0}, \quad \theta = \frac{\bar{T} - \bar{T}_\infty}{\bar{T}_w - \bar{T}_\infty}, \quad \phi = \frac{\bar{C} - \bar{C}_\infty}{\bar{C}_w - \bar{C}_\infty}, \\ Sc &= \frac{\nu}{D}, \quad Pr = \frac{\rho \nu C_P}{\kappa}, \quad Gr = \frac{\nu g \beta (\bar{T}_w - \bar{T}_\infty)}{u_0^3}, \\ Gr_m &= \frac{\nu g \beta (\bar{C}_w - \bar{C}_\infty)}{u_0^3}, \quad t = \frac{u_0^2 \bar{t}}{\nu}, \quad M = \frac{\sigma B_0^2 \nu}{\rho u_0^2}, \\ Ra &= \frac{16 \bar{\alpha} \nu \bar{\sigma} \bar{T}_\infty^3}{\kappa u_0^2}, \quad \omega = \frac{\bar{\omega} \nu}{u_0^2}, \quad Cr = \frac{\nu \bar{C}_r}{u_0^2}, \\ A &= \frac{u_0^2}{\nu}, \quad Kr = \frac{\bar{K}_r u_0^2}{\nu^2} \end{aligned} \quad (8)$$

Using the transformations Eq. (8), the non-dimensional forms of Eq. (1), Eq. (3) and Eq. (7) are

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial y^2} + Gr\theta + Gr_m\phi - (M + Kr^{-1})u \quad (9)$$

$$\frac{\partial \theta}{\partial t} = \frac{1}{Pr} \frac{\partial^2 \theta}{\partial y^2} - \frac{Ra}{Pr} \theta \quad (10)$$

$$\frac{\partial \phi}{\partial t} = \frac{1}{Sc} \frac{\partial^2 \phi}{\partial y^2} - Cr\phi \quad (11)$$

The corresponding initial and boundary conditions are transformed to:

$$\begin{aligned} t \leq 0 : u &= 0, \quad \theta = 0, \quad \phi = 0 \quad \forall y \\ y > 0 : u &= \cos(\omega t), \theta = t, \phi = t \quad \text{at } y = 0 \\ y > 0 : u &\rightarrow 0, \quad \theta \rightarrow 0, \quad \phi \rightarrow 0 \quad \text{as } y \rightarrow \infty \end{aligned} \quad (12)$$

3. METHOD OF SOLUTION

The unsteady, non-linear, coupled partial differential Eq. (9) to Eq. (11) along with their boundary conditions Eq. (12) have been solved analytically using usual Laplace transform technique and the solutions for hydro magnetic flow in the presence of radiation and first order chemical reaction are obtained as follows:

$$\begin{aligned} \theta(y, t) &= \left(\frac{t}{2} + \frac{yPr}{4\sqrt{Ra}}\right) e^{y\sqrt{Ra}} \operatorname{erfc}\left(\eta\sqrt{Pr} + \sqrt{\frac{Ra t}{Pr}}\right) + \left(\frac{t}{2} - \frac{yPr}{4\sqrt{Ra}}\right) e^{y\sqrt{Ra}} \operatorname{erfc}\left(\eta\sqrt{Pr} - \sqrt{\frac{Ra t}{Pr}}\right) \\ &\quad + \sqrt{\frac{Ra t}{Pr}} \end{aligned} \quad (13)$$

$$\begin{aligned} \phi(y, t) &= \left(\frac{t}{2} + \frac{\eta\sqrt{Sc} t}{2\sqrt{Cr}}\right) e^{2\eta\sqrt{Cr} Sc} \operatorname{erfc}(\eta\sqrt{Sc} + \sqrt{Cr} t) + \left(\frac{t}{2} - \frac{\eta\sqrt{Sc} t}{2\sqrt{Cr}}\right) e^{-2\eta\sqrt{Cr} Sc} \operatorname{erfc}(\eta\sqrt{Sc} - \sqrt{Cr} t) \end{aligned} \quad (14)$$

$$\begin{aligned} u(y, t) &= \frac{1}{4} e^{i\omega t} \left[e^{y\sqrt{N+i\omega}} \operatorname{erfc}\left\{\eta + \sqrt{(N-i\omega)t}\right\} + e^{-y\sqrt{N+i\omega}} \operatorname{erfc}\left\{\eta - \sqrt{(N+i\omega)t}\right\} \right] + \frac{1}{4} e^{-i\omega t} \left[e^{y\sqrt{N-i\omega}} \operatorname{erfc}\left\{\eta + \sqrt{(N+i\omega)t}\right\} + e^{-y\sqrt{N-i\omega}} \operatorname{erfc}\left\{\eta - \sqrt{(N-i\omega)t}\right\} \right] - \frac{Q}{2} \left[e^{y\sqrt{M}} \operatorname{erfc}(\eta + \sqrt{Nt}) + e^{-y\sqrt{M}} \operatorname{erfc}(\eta - \sqrt{Nt}) \right] + B \left[\left(\frac{t}{2} + \frac{y}{4\sqrt{N}}\right) e^{y\sqrt{M}} \operatorname{erfc}(\eta + \sqrt{Nt}) + \left(\frac{t}{2} - \frac{y}{4\sqrt{N}}\right) e^{-y\sqrt{M}} \operatorname{erfc}(\eta - \sqrt{Nt}) \right] + \frac{E}{2} e^{ct} \left[e^{y\sqrt{N-C}} \operatorname{erfc}\left\{\eta + \sqrt{(N-C)t}\right\} + e^{-y\sqrt{N-C}} \operatorname{erfc}\left\{\eta - \sqrt{(N-C)t}\right\} \right] + \frac{G}{2} e^{et} \left[e^{y\sqrt{N+e}} \operatorname{erfc}\left\{\eta + \sqrt{(N+e)t}\right\} + e^{-y\sqrt{N+e}} \operatorname{erfc}\left\{\eta - \sqrt{(N+e)t}\right\} \right] + \frac{E}{2} e^{et} \left[e^{y\sqrt{Ra}} \operatorname{erfc}\left\{\eta\sqrt{Pr} + \sqrt{\frac{Ra t}{Pr}}\right\} + e^{-y\sqrt{Ra}} \operatorname{erfc}\left\{\eta\sqrt{Pr} - \sqrt{\frac{Ra t}{Pr}}\right\} \right] + D\theta(y, t) - \frac{E}{2} e^{-ct} \left[e^{y\sqrt{Ra-CPr}} \operatorname{erfc}\left\{\eta\sqrt{Pr} + \sqrt{\left(\frac{Ra}{Pr} - C\right)t}\right\} + e^{-y\sqrt{Ra-CPr}} \operatorname{erfc}\left\{\eta\sqrt{Pr} - \sqrt{\left(\frac{Ra}{Pr} - C\right)t}\right\} \right] + F\phi(y, t) + G\operatorname{erfc}(y\sqrt{Sc}) - \frac{G}{2} \left[e^{y\sqrt{eSc}} \operatorname{erfc}\left\{\eta\sqrt{Sc} + \sqrt{et}\right\} + e^{-y\sqrt{eSc}} \operatorname{erfc}\left\{\eta\sqrt{Sc} - \sqrt{et}\right\} \right] \end{aligned} \quad (15)$$

where $\eta = \frac{y}{2\sqrt{t}}$, $b = \frac{Gr}{Pr-1}$, $C = \frac{Ra-N}{Pr-1}$, $d = \frac{Gr_m}{Sc-1}$, $e = \frac{N}{Sc-1}$, $N = M + Kr^{-1}$, $Q = \frac{Gr(Pr-1)}{(Ra-N)^2} + \frac{Gr_m(Sc-1)}{M^2}$, $B = \frac{M(Gr+Gr_m) - RaGr_m}{N(Ra-N)}$, $D = \frac{Gr}{Ra-N}$, $E = \frac{Gr(Pr-1)}{(Ra-N)^2}$, $F = \frac{Gr_m}{N}$, $G = Gr_m \left(\frac{Sc-1}{N}\right)^2$.

4. SKIN FRICTION

The boundary layer produces a drag force on the plate due to the viscous stresses which are developed at the wall. The viscous stress at the surface of the plate is given by

$$\begin{aligned} \tau &= -\left[\frac{\partial u(y, t)}{\partial y}\right]_{y=0} = \frac{1}{2} \left[e^{i\omega t} \left\{ \frac{e^{-(N+i\omega)t}}{\sqrt{\pi t}} + \sqrt{(N+i\omega)t} \operatorname{erf}(\sqrt{(N+i\omega)t}) \right\} + e^{-i\omega t} \left\{ \frac{e^{-(N-i\omega)t}}{\sqrt{\pi t}} + \sqrt{(N-i\omega)t} \operatorname{erf}(\sqrt{(N-i\omega)t}) \right\} \right] + e^{-ct} \left[\frac{e^{-(N-C)t}}{\sqrt{\pi t}} + \sqrt{N-C} \operatorname{erf}(\sqrt{(N-C)t}) \right] + G e^{et} + E \left[\sqrt{\frac{Pr}{\pi t}} e^{-Ra t/Pr} + \sqrt{Ra} \operatorname{erf}\left(\sqrt{\frac{Ra t}{Pr}}\right) \right] - D \left[t\sqrt{Ra} \operatorname{erf}\left(\sqrt{\frac{Ra t}{Pr}}\right) + \right] \end{aligned} \quad (16)$$

$$\sqrt{\frac{tPr}{\pi}} e^{-Ra t/Pr} + \frac{Pr}{2\sqrt{Ra}} \operatorname{erf}\left(\sqrt{\frac{Ra t}{Pr}}\right) -$$

$$E e^{Ct} \left[\sqrt{\frac{Pr}{\pi t}} e^{-Ra t/Pr} + \right.$$

$$\left. \sqrt{Ra} - CPr \operatorname{erf}\left(\sqrt{\frac{Ra t}{Pr}}\right) \right] + G \sqrt{\frac{Sc}{\pi t}} + 2F \sqrt{\frac{tSc}{\pi}} -$$

$$G e^{et} \left[\sqrt{\frac{Sc}{\pi t}} e^{-et} + \sqrt{eSc} \operatorname{erf}(\sqrt{et}) \right]$$

5. NUMERICAL TECHNIQUE

In order to solve the unsteady, non-linear coupled Eq. (9) to Eq. (11) under the conditions Eq. (12), an implicit finite difference scheme of the Crank-Nicolson type has been employed. The finite difference equations corresponding to Eq. (9) to Eq. (11) are as follows:

$$\frac{[u_{i,j}^{n+1} - u_{i,j}^n]}{\Delta t} = \frac{1}{2(\Delta y)^2} [u_{i,j-1}^{n+1} - 2u_{i,j}^{n+1} + u_{i,j+1}^{n+1} +$$

$$u_{i,j-1}^n - 2u_{i,j}^n + u_{i,j+1}^n] + \frac{Gr [\theta_{i,j}^{n+1} + \theta_{i,j}^n]}{2} + \quad (17)$$

$$\frac{Gr_m [\phi_{i,j}^{n+1} + \phi_{i,j}^n]}{2} - \frac{[u_{i,j}^{n+1} + u_{i,j}^n]}{2} (M + K^{-1})$$

$$\frac{[\theta_{i,j}^{n+1} - \theta_{i,j}^n]}{\Delta t} =$$

$$\frac{[\theta_{i,j-1}^{n+1} - 2\theta_{i,j}^{n+1} + \theta_{i,j+1}^{n+1} + \theta_{i,j-1}^n - 2\theta_{i,j}^n + \theta_{i,j+1}^n]}{2 Pr (\Delta y)^2} -$$

$$\frac{Ra [\theta_{i,j}^{n+1} + \theta_{i,j}^n]}{2 Pr} \quad (18)$$

$$\frac{[\phi_{i,j}^{n+1} - \phi_{i,j}^n]}{\Delta t} =$$

$$\frac{[\phi_{i,j-1}^{n+1} - 2\phi_{i,j}^{n+1} + \phi_{i,j+1}^{n+1} + \phi_{i,j-1}^n - 2\phi_{i,j}^n + \phi_{i,j+1}^n]}{2 Sc (\Delta y)^2} -$$

$$\frac{C_r [\phi_{i,j}^{n+1} + \phi_{i,j}^n]}{2 Sc} \quad (19)$$

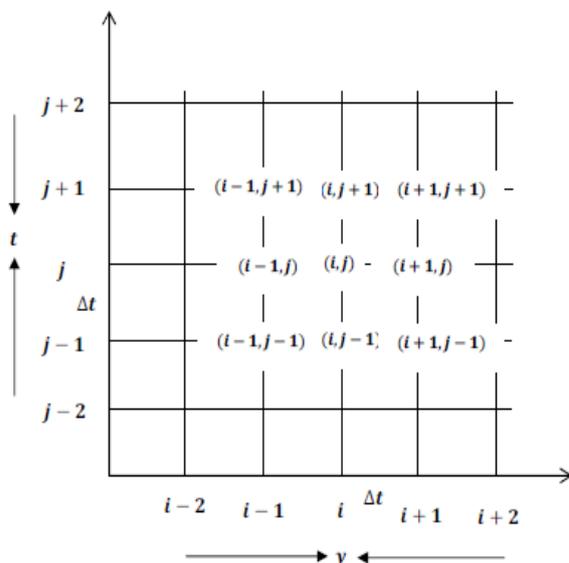


Fig. 2. Finite difference space grid

The region of integration is considered as a rectangle with sides $x_{max}(= 1)$ and $y_{max}(= 14)$, where y_{max} corresponds to $y = \infty$ which lies very well outside both the momentum and energy boundary layers. The maximum of y was chosen as 14 after some preliminary

investigations so that the last two of the boundary conditions (14) are satisfied within the tolerance limit 10^{-5} . After experimenting with a few set of mesh sizes, the mesh sizes have been fixed at the level $\Delta y = 0.25$ with time step $\Delta t = 0.01$. In this case, the spatial mesh sizes are reduced by 50% in one direction, and later in both directions, and the results are compared. It is observed that, when the mesh size is reduced by 50% in the y -direction, the results differ in the fifth decimal place while the mesh sizes are reduced by 50% in x -direction or in both directions; the results are comparable to three decimal places.

Hence, the above mesh sizes have been considered as appropriate for calculation. The coefficients $u_{i,j}^n$ and $v_{i,j}^n$ appearing in the finite-difference equations are treated as constants in any one time step. Here i - designates the grid point along the x -direction, j along the y -direction. The values of u, v and θ are known at all grid points at $t = 0$ from the initial conditions.

The computations of u, v, θ and ϕ at time level $(n + 1)$ using the values at previous time level (n) are carried out as follows: The finite difference Eq. (19) at every internal nodal point on a particular i -level constitutes a tri-diagonal system of equations. Such systems of equations are solved by using Thomas algorithm as discussed in Carnahan *et al.* (1969). Thus, the values of ϕ are found at every nodal point for a particular i at $(n + 1)^{th}$ time level. Similarly, the values of θ are calculated from Eq. (18). Using the values of ϕ and θ at $(n + 1)^{th}$ time level in the Eq. (17), the values of u at $(n + 1)^{th}$ time level are found in a similar manner. Thus, the values of ϕ, θ and u are known on a particular i -level. This process is repeated for various i -level. Thus the values of ϕ, θ, u are known, at all grid points in the rectangular region at $(n + 1)^{th}$ time level.

In a similar manner, computations are carried out by moving along the i -direction. After computing values corresponding to each i at a time level, the values at the next time level are determined in a similar manner. Computations are repeated until the steady-state is reached. The steady state solution is assumed to have been reached, when the absolute difference between the values of u , as well as temperature θ and concentration ϕ at two consecutive time steps are less than 10^{-5} at all grid points.

5.1 Stability Analysis

The stability criterion of the finite difference scheme for constant mesh sizes are examined using Von-Neumann technique as explained by Carnahan *et al.* (1969). The general term of the Fourier expansion for u, θ and ϕ at a time arbitrarily called $t = 0$, are assumed to be of the form $\exp(i\beta y)$ (here $i = \sqrt{-1}$). At a later time t , these terms will become,

$$u = H_1(t) \exp(i\beta y)$$

$$\theta = H_2(t) \exp(i\beta y) \quad (20)$$

$$\phi = H_3(t) \exp(i\beta y)$$

Substituting Eq. (20) in Eq. (17) to Eq. (19) under the assumption that the coefficients u, θ and ϕ are constants over any one time step and denoting the values after one time step by H_1', H_2' and H_3' . After simplification, we get

$$\frac{H_1' - H_1}{\Delta t} = \frac{(H_2' + H_2)Gr + (H_3' + H_3)Gr_m}{(\Delta y)^2} + (H_1' + H_1) \left[\frac{\cos(\beta \Delta y) - 1}{(\Delta y)^2} - \frac{(M+K^{-1})}{2} \right] \quad (21)$$

$$\frac{H_2' - H_2}{\Delta t} = \left[\frac{\cos(\beta \Delta y) - 1}{(\Delta y)^2} - \frac{Ra}{2} \right] \frac{(H_2' + H_2)}{Pr} \quad (22)$$

$$\frac{H_3' - H_3}{\Delta t} = \left[\frac{\cos(\beta \Delta y) - 1}{(\Delta y)^2} - \frac{C_r}{2} \right] \frac{(H_3' + H_3)}{Sc} \quad (23)$$

Equations (21) to (23) can be rewritten as,

$$(1 + I)H_1' = (1 - I)H_1 + \frac{\Delta t}{2} [Gr(H_2' + H_2) + Gr_m(H_3' + H_3)] \quad (24)$$

$$(1 + J)H_2' = (1 - J)H_2 \quad (25)$$

$$(1 + L)H_3' = (1 - L)H_3 \quad (26)$$

where

$$I = [1 - \cos(\beta \Delta y)] \frac{\Delta t}{(\Delta y)^2} + \frac{(M+K^{-1})\Delta t}{2},$$

$$J = [1 - \cos(\beta \Delta y)] \frac{\Delta t}{Pr (\Delta y)^2} + \frac{Ra \Delta t}{2Pr}$$

$$L = [1 - \cos(\beta \Delta y)] \frac{\Delta t}{Sc (\Delta y)^2} + \frac{C_r \Delta t}{2Sc}.$$

After eliminating H_2' and H_3' in Eq. (24) using Eq. (25) and Eq. (26), the resultant equation is given by,

$$(1 + I)H_1' = (1 - I)H_1 + H_2 \frac{Gr \Delta t}{(1+J)} + H_3 \frac{Gr_m \Delta t}{(1+L)} \quad (27)$$

Equations (27) to (29) can be written in matrix form as follows:

$$\begin{pmatrix} H_1' \\ H_2' \\ H_3' \end{pmatrix} = \begin{pmatrix} \frac{1-I}{1+I} & P_1 & P_2 \\ 0 & \frac{1-J}{1+J} & 0 \\ 0 & 0 & \frac{1-L}{1+L} \end{pmatrix} \begin{pmatrix} H_1 \\ H_2 \\ H_3 \end{pmatrix} \quad (28)$$

where $P_1 = \frac{Gr \Delta t}{(1+I)(1+J)}$ and $P_2 = \frac{Gr_m \Delta t}{(1+I)(1+L)}$.

Now, for stability of the finite difference scheme, the modulus of each Eigen value of the amplification matrix does not exceed unity. Since the matrix Eq. (28) is triangular, the Eigen values are its diagonal elements. The Eigen values of the amplification matrix are $(1 - I)/(1 + I)$, $(1 - J)/(1 + J)$ and $(1 - L)/(1 + L)$.

Assuming that, u is everywhere non-negative and v is everywhere non-positive, we get

$$I = 2 \frac{\Delta t}{(\Delta y)^2} \sin^2 \left(\frac{\beta \Delta y}{2} \right) + \frac{(M+K^{-1})}{2} \Delta t$$

Since the real part of A is greater than or equal to zero, $|(1 - I)/(1 + I)| \leq 1$ always. Similarly, $|(1 - J)/(1 + J)| \leq 1$ and $|(1 - L)/(1 + L)| \leq 1$. Hence, the finite difference scheme is unconditionally stable. The local truncation error is $O(\Delta t^2 + \Delta y^2)$ and it tends to zero as Δt and Δy tend to zero. Hence, the scheme is compatible. Stability and compatibility ensures convergence.

5.2 Accuracy

We have obtained a comprehensive range of solutions to the transformed conservation equations. To test the validity of numerical Crank Nicolson computations, we have compared the flow velocity and Concentration distributions in Tables 1 and Table 2 with the Laplace transform solutions. It is clearly seen from Table 1 and Table 2 that the results are in excellent agreement. As the accuracy of the numerical solutions is very good, the values of u and ϕ corresponding to analytical and numerical solutions are very close to each other. Table 1 shows that the flow velocity is found to accelerate with free convection parameter G from 0.0 through 5.0 to 10.0. On the other hand, increasing the Schmidt number Sc from 0.30 through 0.60 to 0.78 the Concentration distribution is found to depress (Table 2).

Table 1 Comparison of values of the flow velocity (u) for the present results (Laplace Technique and Crank Nicolson Method) with $Gr_m = 5, Ra = 2, K = 0.2, Sc = 0.78, M = 5.0, t = 0.5$ and $Pr = 0.71$

<i>Laplace Technique</i>			
	<i>Gr</i>		
y	0.0	5.0	10.0
0.0	1	1	1
2.0	4.173150	4.573802	4.941724
4.0	0.401362	0.438209	0.461072
6.0	0.074019	0.084105	0.098704
8.0	0.005317	0.007518	0.009371
10.0	0.000852	0.000952	0.002504
<i>Crank Nicolson Method</i>			
	<i>Gr</i>		
y	0.0	5.0	10.0
0.0	1	1	1
2.0	4.174024	4.573983	4.942107
4.0	0.402033	0.438571	0.461310
6.0	0.075105	0.084791	0.098872
8.0	0.005451	0.007619	0.009502
10.0	0.000863	0.000971	0.002514

Table 2 Comparison of values of the Concentration (ϕ) for the present results (Laplace Technique and Crank Nicolson Method) with $t = 1.5, C_r = 1$:

Laplace Technique			
	Sc		
y	0.30	0.60	0.78
0.0	1.000000	1.000000	1.000000
2.0	0.347031	0.317402	0.284172
4.0	0.118063	0.075043	0.038730
6.0	0.024571	0.006527	0.002743
8.0	0.003620	0.001209	0.000451
10.0	0.000852	0.000372	0.000085
Crank Nicolson Method			
	Sc		
y	0.30	0.60	0.78
0.0	1.000000	1.000000	1.000000
2.0	0.348051	0.317541	0.284308
4.0	0.118131	0.075170	0.038855
6.0	0.024618	0.006617	0.002782
8.0	0.003704	0.001314	0.000507
10.0	0.000867	0.000383	0.000091

6. RESULTS AND DISCUSSION

To gain a perspective of the physics of the flow regime, we have numerically evaluated the effects of Hartmann number (M), radiation-conduction parameter (R_a), dimensionless time (t), porosity parameter (K_r) and chemical reaction parameter (C_r), on the velocity, u , temperature, θ , shear stress function, $\frac{\partial u}{\partial y}|_{y=0}$. Here we consider $Gr = 5 = Gr_m > 0$ (cooling of the plate) i.e. free convection currents convey heat away from the plate in to the boundary layer, $t = 0.5, R_a = 10$ throughout the discussion. The Prandtl number Pr is taken for air at 20 °C ($Pr = 0.71$), electrolytic solution ($Pr = 1.0$) and water ($Pr = 7.0$).

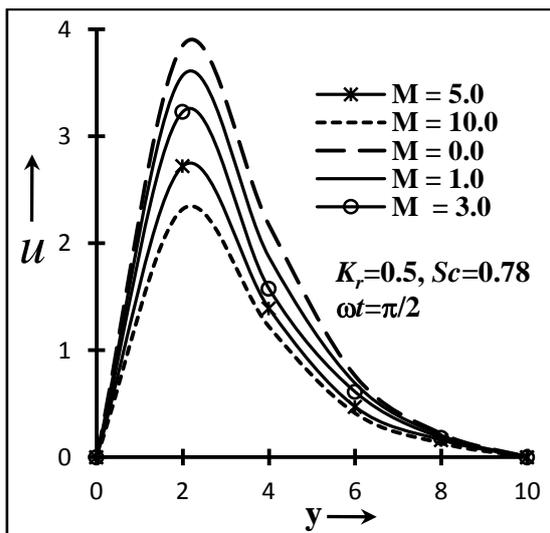


Fig. 3. Flow velocity for Hartmann number

In Fig. 3 we have presented the influence of Hartmann number square root M on the velocity u distributions with distance normal to the plate (transverse

coordinate, y). The hydromagnetic term in the dimensionless equation (2.9), $-Mu$ is a linear drag force term. With increasing magnetic field strength, B_0 , M is increased and this serves to decelerate the flow along the plate. In accordance with this, we observe in Fig. 3 that u profile values are strongly reduced with increasing M . We also note that as M rises, the profiles decay to zero progressively for shorter distances from the plate surface. The strong inhibiting effect of magnetic field is therefore evident. Also it is noticed that the velocity distribution increases with the increase in time parameter.

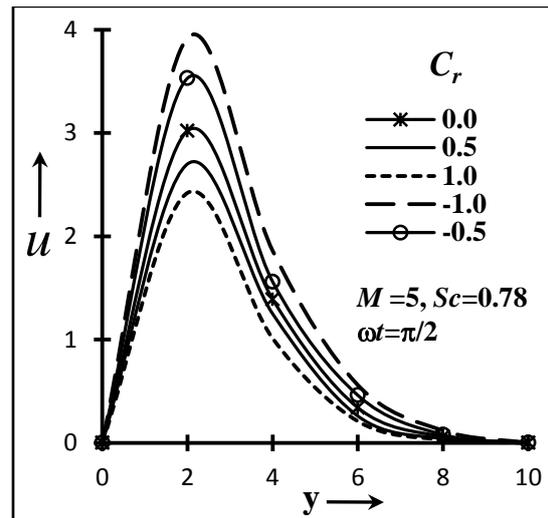


Fig. 4. Flow velocity for chemical reaction

Figures 4 and 5 display the effects of the chemical reaction parameter C_r on the velocity u and concentration ϕ profiles, respectively. As expected, the presence of the chemical reaction significantly affects the concentration profiles as well as the velocity profiles. It should be mentioned that the studied case is both for destructive ($C_r > 0$) and generative ($C_r < 0$) chemical reaction. In fact, as ($C_r > 0$) increases, the considerable reduction in the velocity profiles is predicted, and the presence of the peak indicates that the maximum value of the velocity occurs in the body of the fluid close to the surface but not at the surface. Also, with an increase in the chemical reaction parameter, the concentration decreases. It is evident that the increase in the chemical reaction C_r significantly alters the concentration boundary layer thickness but does not alter the momentum boundary layers. Moreover, these results are observed to be opposite for the case of ($C_r < 0$).

The effect of time (t) and radiation-conduction parameter R_a on spatial distribution of the dimensionless temperature function (θ) is shown in Fig. 6. Temperature is seen to decrease from a maximum value at the wall (1.0) to a minimum value with maximum distance, y . However with increasing time (t) we observe that there is a clear increase in temperatures. This trend is maintained at all locations in the flow regime. At fixed time, $t = 0.2$, an increase in thermal radiation-conduction parameter (R_a) is observed to strongly increase temperatures throughout the fluid with

distance normal to the wall in the fluid regime. Larger (R_a) values correspond to an increased dominance of thermal radiation over conduction. As such thermal radiation supplements the thermal diffusion and increases the overall thermal diffusivity of the regime since the local radiant diffusion flux model adds radiation conductivity to the conventional thermal conductivity. As a result the temperatures in the fluid regime flow are significantly increased.

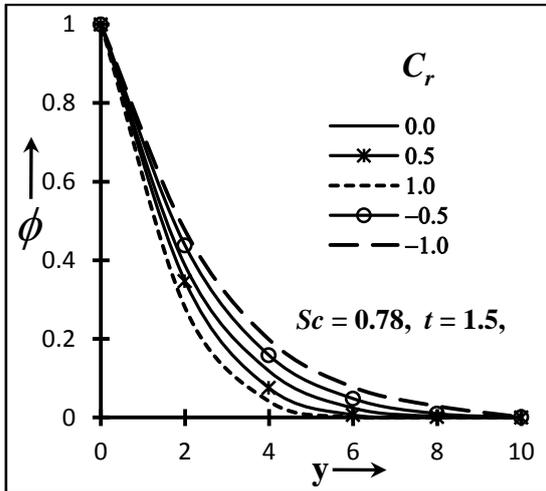


Fig. 5. Concentration for chemical reaction

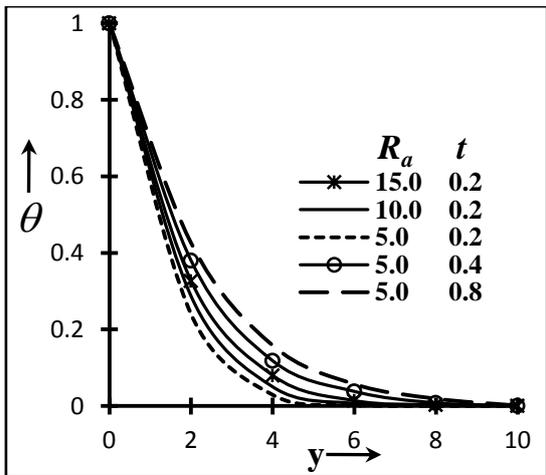


Fig. 6. Temperature for radiation and time

In Fig.7 the collective influence of the thermal radiation-conduction parameter (R_a) on the shear stress function variation against Hartmann number is shown. Increasing M clearly increases shear stress function $\left. \frac{\partial u}{\partial y} \right|_{y=0}$ values. Similarly in consistency with previous computations, an increase in thermal radiation also serves to accelerate the flow which increases shear stress function values i.e. the maximum shear stress function, $\left. \frac{\partial u}{\partial y} \right|_{y=0}$, corresponds to the maximum M value (highest magnetic body force).

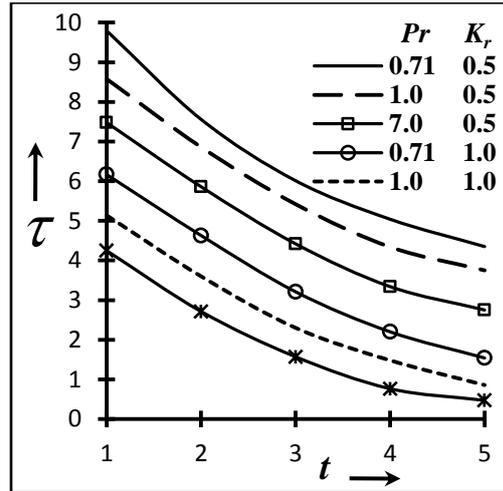


Fig. 7. Skin friction for porosity and Pr

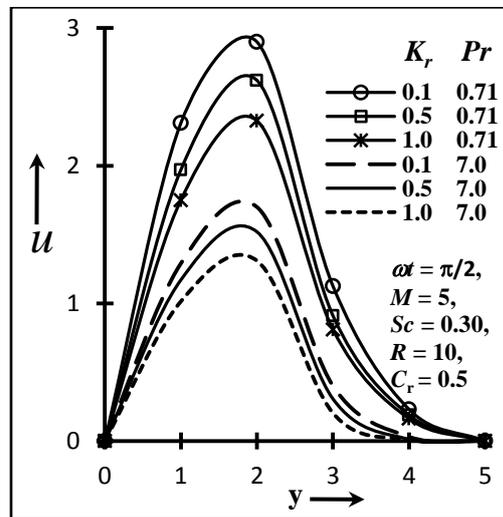


Fig. 8. Flow velocity for porosity and Pr

Figure 8 reveals the effects of K_r on the velocity profiles. The presence of a porous medium increases the resistance to flow resulting in decrease in the flow velocity. This behavior is depicted by the decrease in the velocity as K_r decreases for both air and water. The magnitude of velocity for air is higher than that of water.

Figure 9 shows the skin-friction against time t for various values of parameters Pr and K_r . It is observed that as time passes the skin friction decreases. The skin-friction decreases with increasing permeability parameter K_r for both air and water. The magnitude of the skin-friction for water is greater than that for air ($Pr = 0.71$) and electrolytic solution ($Pr = 1.0$).

Figure 10 illustrate the temperature (θ) profiles for different Prandtl numbers Pr . The results show that the increasing Prandtl number results in a decrease in the thermal boundary layer and in general lower average temperature within the boundary layer. The reason is that smaller Pr is equivalent to the increase in the thermal conductivity of the fluid, and heat is able to diffuse away from the heated surface more rapidly for higher values of Pr . Therefore, in the case of smaller

Prandtl numbers, the thermal boundary layers thicker, and the rate of heat transfer is reduced.

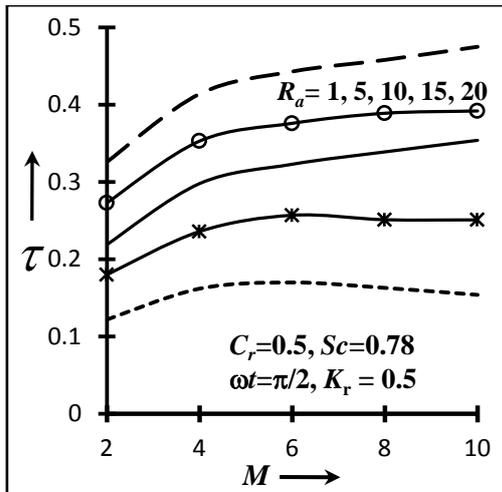


Fig. 9. Skin friction for R_a and M number

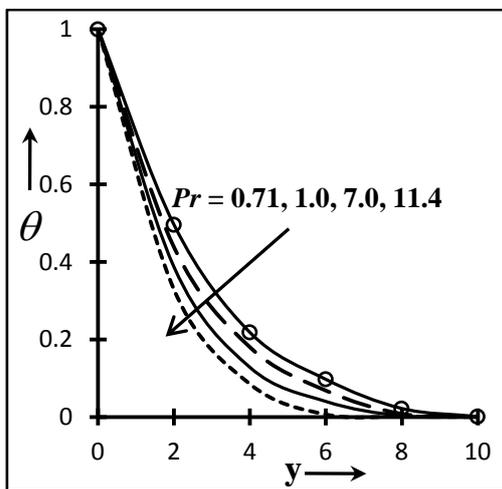


Fig. 10. Temperature distributions for Pr

7. CONCLUSION

A mathematical analysis has been presented of the transient free convection-radiation magneto hydrodynamic viscous flow along an infinite vertical permeable plane under a transverse magnetic field in presence of chemical reaction. A flux model has been employed to simulate thermal radiation effects, valid for optically-thick gases. The dimensionless momentum, energy and mass conservations equations have been solved using both the Laplace transform technique and Numerical Crank Nicolson method. The study has shown that the flow is accelerated with a decrease in Hartmann number square root (M). The velocity as well as the concentration decreases with an increase in the chemical reaction parameter. Temperature of the gas is shown to be enhanced both with the elapse of time (t) and increasing conduction-radiation (R_a) i.e. greater thermal radiation heat transfer contribution. The current study has employed a Newtonian viscous model. Presently the authors are extending this work to examine several non-Newtonian fluids of interest in

glass rheological thermal processing including viscoelastic models; the results of these investigations will be communicated imminently.

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