

Hydromagnetic Flow over an Inclined Non-Linear Stretching Sheet with Variable Viscosity in the Presence of Thermal Radiation and Chemical Reaction

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ABSTRACT

An analysis has been made to investigate the effects of thermal radiation on the magnetohydrodynamic (MHD) flow and heat transfer over an inclined non-linear stretching sheet. The surface velocity of the stretching sheet and the transverse magnetic field are assumed to vary as a power function of the distance from the origin. The effect of internal heat generation/absorption is taken into account. The fluid viscosity is assumed to vary as an inverse linear function of temperature. A generalized similarity transformation is used to reduce the governing partial differential equations to a system of non-linear coupled ordinary differential equations, and is solved numerically by using a finite difference scheme. The numerical results concerned with the velocity, temperature and concentration distributions as well as the skin-friction coefficient and the Nusselt number for various values of the dimensionless parameters of interest are obtained. Some important findings reported in this paper reveal that the effect of thermal radiation and heat generation/absorption have significant role in controlling the rate of heat transfer in the boundary layer region.

Keywords: Thermal radiation, Chemical reaction, Variable viscosity, Inclined sheet.

NOMENCLATURE

a, T_r	constants	Re_x	local Reynolds number
B_0	constant magnetic field strength	Sc	Schmidt number
C	dimensional concentration variable	T	dimensional temperature variable
C_w	concentration at the sheet	T_∞	free stream temperature
C_f	skin-friction coefficient	T_w	temperature at the sheet
C_p	specific heat at constant pressure	U_w	surface velocity of the sheet
D	molecular diffusivity	u, v	dimensional velocity components
E_c	Eckert number	α	angle of inclination
f	dimensionless stream function	β	nonlinear stretching parameter
Gr_t	Grashof number	β_t	thermal expansion coefficient
Gr_c	Modified Grashof number	β_c	concentration expansion coefficient
g_0	acceleration due to gravity	λ	heat generation/ absorption parameter
K	mean absorption coefficient	σ^*	Stefan-Boltzmann constant
k	thermal conductivity	σ	electrical conductivity
k_0	reaction rate constant	ψ	dimensional stream function
M	magnetic parameter	η	non-dimensional distance
Nr	thermal radiation parameter	θ	dimensionless temperature
Nu	Nusselt number	ϕ	dimensionless concentration
n	power index	μ	coefficient of viscosity
Pr	Prandtl number	ρ_∞	density of the free stream
Q	heat source/sink	θ_r	viscosity parameter

q_r heat flux γ chemical reaction parameter

1. INTRODUCTION

The boundary layer flow over a nonlinear stretching sheet has been the recent topic of researchers and engineers, because of its many engineering and industrial applications. The investigation of the boundary-layer flows and heat transfer of an incompressible fluid over an inclined stretching surface has also many important applications such as the extrusion of plastic sheets from a die, the boundary layer along a liquid film condensation process, gas turbines, MHD power generators, the cooling process of metallic plate in a cooling bath, in the glass and polymer industries, flight magnetohydrodynamics as well as in the field of planetary magnetosphere, aeronautics and chemical engineering. The rate of heat transfer at the stretching sheet plays a vital role to obtain better quality of the final product. If the temperature of the surrounding fluid becomes high, then the thermal radiation effect has a significant impact in the case of space technology. The effects of mass transfer with chemical reaction on the boundary layer flow has enormous applications in chemical engineering processes such as to enhanced oil recovery, packed-bed catalytic reactors, solidification of binary alloy as well as catalytic surface reactions in hydrodynamic flows.

Sakiadis (1961) initiated the study of boundary layer flow on a continuous moving surface. Later on Crane (1970) extended this problem to a stretching sheet whose surface velocity varies linearly with the distance x from the fixed point. Consequently Gupta and Gupta (1977) examined the heat and mass transfer over a linear stretching sheet subjected to suction/blowing. The influence of uniform magnetic field on the flow of an electrically conducting fluid past a stretching sheet have been investigated by Pavlov (1974), Andersson (1992), Watanabe and Pop (1993, 1995), Shit (2009), Prasad *et al.* (2010) and Shit and Haldar (2012a). Afify (2004) investigated the chemical reaction on free convective flow and mass transfer of a viscous, incompressible and electrically conducting fluid over a stretching sheet in the presence of a uniform transverse magnetic field. Misra and Shit (2008) extensively studied on electrically conducting fluid flow and heat transfer in a parallel plate channel with stretching walls in the presence of a magnetic field applied externally. Two-dimensional unsteady MHD flow of a viscous fluid between two moving parallel plates has been investigated by Sweet *et al.* (2011). Jafar *et al.* (2012) carried out the steady magnetohydrodynamic (MHD) laminar boundary layer flow of a viscous and incompressible electrically conducting fluid near the stagnation point on a horizontal stretching or shrinking surface, with variable surface temperature and a constant magnetic field applied normal to the surface of the sheet.

Recently, a new idea is added to the study of boundary layer fluid flow and heat transfer is the consideration of the effect of thermal radiation and temperature dependent viscosity. Many processes in engineering applications occur at high temperature and the radiated

heat transfer becomes very important for the design of the pertinent equipment. Motivated by these assumptions, Shit and Haldar (2011a, 2012b) examined the combined effects of thermal radiation and hall current on momentum, heat and mass transfer in the laminar boundary layer fluid flow over an inclined permeable stretching sheet with variable viscosity. Tak *et al.* (2010) investigated the interaction of radiation with free convection in Darcian porous media by taking into account the Soret and Dufour's effects. Nonlinear hydromagnetic flow over a stretching surface with prescribed heat and mass flux embedded in a porous medium have analyzed analytically by Anjalidevi and Kayalvizhi (2013). Mukhopadhyaya *et al.* (2005) investigated the problem of MHD boundary layer flow over a heated stretching sheet with variable viscosity. But, Salem (2007) investigated the effect of variable viscosity on MHD viscoelastic fluid flow and heat transfer over a stretching sheet without considering the effect of thermal radiation. Moreover, an analytical solution was obtained by Fang and Zhang (2010) for the flow and heat transfer over a linear shrinking sheet with mass transfer, wherein the effects of thermal radiation and variable thermal conductivity have been neglected. However, all the above studies are restricted in a linear stretching sheet.

Vajravelu and Cannon (2006) numerically examined the effects of nonlinearly stretching sheet on the flow characteristics of viscous incompressible fluid. Prasad *et al.* (2013) have investigated the effects of internal heat generation/absorption, thermal radiation, magnetic field and temperature-dependent thermal conductivity on the flow and heat transfer characteristics of a Non-Newtonian fluid over a stretching sheet. To characterize the non-Newtonian fluid behavior they have used upper convected Maxwell (UCM) fluid model. The numerical results for the physical variables have been obtained by using finite difference scheme along with the Keller-Box method. Mostafa *et al.* (2011) carried out the magnetohydrodynamic boundary layer flow and heat transfer of an electrically conducting micropolar fluid over a nonlinear stretching surface with variable wall heat flux in the presence of heat generation/absorption. Shit and Haldar (2011b) numerically investigated the effects of thermal radiation and variable fluid properties on the MHD fluid flow over a nonlinear porous shrinking sheet.

In this paper, we study the effects of thermal radiation and chemical reaction on the MHD fluid flow over a non-linear inclined stretching sheet with variable viscosity in the presence of heat generation /absorption. The viscous dissipation and buoyancy effects are taken into account in a situation when there is a temperature dependent viscosity. The present problem pertains to a situation in which the chemical reaction takes place. Since the governing differential equations are highly non-linear, Newton's linearization method is used followed by the finite difference scheme to obtain numerical solutions. The numerical results of the flow characteristics are presented graphically.

2. MATHEMATICAL FORMULATION AND FLOW ANALYSIS

Let us consider the steady two-dimensional MHD flow and heat transfer along with the chemical reaction phenomenon of an incompressible, viscous and electrically conducting fluid past over an inclined non-linear stretching sheet.

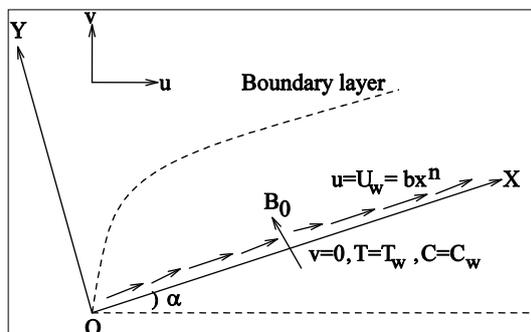


Fig. 1. A physical sketch of the problem

A uniform strong magnetic field of strength B_0 is imposed along the perpendicular to the sheet (Fig.1). The x-axis is assumed to be the direction of the flow and y-axis is normal to it. The temperature and the species concentration are maintained at a prescribed constant value T_w and C_w at the sheet and T_∞ and C_∞ are the fixed values far away from the sheet.

The continuous stretching surface is assumed to have a Power-law velocity $u=U_w=bx^n$, where $b > 0$ is a constant, x denotes the distance from the slit, n is the power index and U_w represents the surface velocity of the sheet. We consider that electrically conducting fluid is influenced by the applied magnetic field $B(x)$ normal to the stretching sheet. The strength of the magnetic

field $B(x)$ is taken as $B(x) = B_0 x^{\frac{n-1}{2}}$ in which B_0 represents the constant magnetic field strength perpendicular to the sheet. We assume that the induced magnetic field produced by the motion of an electrically conducting fluid is negligible, since there is no electric field because of the negligible polarization of charges. The effect of induced magnetic field can also be neglected because of the low electrical conductivity of the fluid which in turn produces low magnetic Reynolds number.

According to the research conducted by Lai and Kulacki (1990), the fluid viscosity is assumed to vary as a reciprocal of a linear function of the temperature given by

$$\frac{1}{\mu} = \frac{1}{\mu_\infty} [1 + \gamma_0 (T - T_\infty)] \quad \text{i.e.} \quad \frac{1}{\mu} = a(T - T_r) \quad (1)$$

where $a = \frac{\gamma_0}{\mu_\infty}$, $T_r = T_\infty - \frac{1}{\gamma_0}$

In Eq. (1), both a and T_r are constants and their values depend on the thermal property of the fluid, i.e., γ_0 . In general $a > 0$ represents for liquid, whereas $a < 0$ represents gas.

By assuming Rosseland approximation for radiation, the radiative heat flux q_r is given by

$$q_r = -\frac{4\sigma^*}{3K} \frac{\partial T^4}{\partial y} \quad (2)$$

where σ^* is defined as the Stefan-Boltzman constant and K is the mean absorption coefficient. The temperature differences within the flow are so small under the consideration that T^4 may be expressed as linear function of the temperature. Expanding T^4 in a Taylor series about T_∞ and neglecting the higher order terms, we obtain

$$T^4 \cong 4T_\infty^3 T - 3T_\infty^4 \quad (3)$$

Substituting Eq. (4) in Eq. (3) yields

$$\frac{\partial q_r}{\partial y} = -\frac{16\sigma^* T_\infty^3}{3K^*} \frac{\partial^2 T}{\partial y^2} \quad (4)$$

Owing to the above mentioned assumptions, the boundary layer flow over a non-linear stretching sheet is governed by the following system of equations

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (5)$$

$$\rho_\infty \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = \frac{\partial}{\partial y} \left(\mu \frac{\partial u}{\partial y} \right) + \rho_\infty g_0 [\beta_t (T - T_\infty) + \beta_c (c - c_\infty)] \cos \alpha - \sigma B(x)^2 u \quad (6)$$

$$\rho_\infty C_p \left(u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = k \frac{\partial^2 T}{\partial y^2} + \sigma B(x)^2 u^2 + \mu \left(\frac{\partial u}{\partial y} \right)^2 - Q(T - T_\infty) - \frac{\partial q_r}{\partial y} \quad (7)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D \frac{\partial^2 C}{\partial y^2} - K_0 (C - C_\infty) \quad (8)$$

where u and v are the velocity components along the x and y directions respectively, μ is the coefficient of viscosity, g_0 the acceleration due to gravity, β_t the coefficient of thermal expansion, β_c the coefficient of expansion with concentration, α the angle of inclination of the stretching sheet with the horizontal line. T and C are the temperature and concentration variable respectively, D the thermal molecular diffusivity, k_0 is the reaction rate constant, C_p is the specific heat at constant pressure, k is the thermal conductivity, T_∞ and ρ_∞ are the free stream temperature and density. The term $Q(T - T_\infty)$ on the right hand side of Eq. (7) represents the amount of heat generated or absorbed per unit volume. The source term represents the heat source when $Q < 0$ and heat sink when $Q > 0$.

The boundary conditions for the present problem can be written as

$$u = U_w = bx^n, \quad v = 0, \quad T = T_w, \quad C = C_w \quad \text{at } y = 0 \quad (9)$$

$$u \rightarrow 0, \quad T \rightarrow T_\infty, \quad C \rightarrow C_\infty \quad \text{as } y \rightarrow \infty \quad (10)$$

Let us introduce the following similarity transformations as

$$\begin{aligned} \psi(x, y) &= \sqrt{\frac{2\nu bx^{n+1}}{n+1}} f(\eta), \\ u = \frac{\partial \psi}{\partial y} &= bx^n f'(\eta), \\ v = -\frac{\partial \psi}{\partial x} &= -\sqrt{\frac{b\nu(n+1)}{2}} x^{\frac{n-1}{2}} \left\{ f(\eta) + \frac{n-1}{n+1} \eta f'(\eta) \right\}, \\ \eta &= \frac{\sqrt{b(n+1)}}{2\nu} x^{\frac{n-1}{2}} y, \\ \theta(\eta) &= \frac{T - T_\infty}{T_w - T_\infty}, \\ \phi(\eta) &= \frac{C - C_\infty}{C_w - C_\infty} \end{aligned} \quad (11)$$

where ψ and f represent the dimensional and non-dimensional stream function respectively, $\nu = \frac{\mu}{\rho_\infty}$ the kinematic viscosity, η is a similarity space variable in non-dimensional form, θ and ϕ are the dimensionless temperature and concentration.

Clearly, the continuity Eq. (5) is satisfied by u and v defined in Eq. (11). Substitution of Eq. (11) in Eq. (6) to Eq. (8) yields

$$\begin{aligned} f'''' + \beta \frac{\theta - \theta_r}{\theta_r} (f')^2 - \frac{\theta - \theta_r}{\theta_r} f f'' - \frac{\theta'}{\theta - \theta_r} f'' - \frac{\theta - \theta_r}{\theta_r} (2 - \beta) \cos \alpha [Gr_t \theta + Gr_c \phi] + M \left(\frac{\theta - \theta_r}{\theta_r} \right) f' = 0 \end{aligned} \quad (12)$$

$$\begin{aligned} (3N_r + 4)\theta'' + 3N_r P_r f \theta' + 3E_c N_r P_r M (f')^2 - 3\lambda N_r P_r \theta - \left(\frac{\theta_r}{\theta - \theta_r} \right) 3N_r P_r E_c (f')^2 = 0 \end{aligned} \quad (13)$$

$$\phi'' + Sc(f\phi' - \gamma\phi) = 0 \quad (14)$$

and the transformed boundary conditions are given by

$$f'(0) = 1, f(0) = 0, \theta(0) = 1, \phi(0) = 1, \text{ at } \eta = 0 \quad (15)$$

$$f'(\eta) \rightarrow 0, \theta(\eta) \rightarrow 0, \phi(\eta) \rightarrow 0 \text{ when } \eta \rightarrow \infty \quad (16)$$

where primes denote differentiation with respect to η only.

The dimensionless parameter appeared in Eq. (12) to Eq. (14) are defined as $\theta_r = \frac{T_r - T_\infty}{T_w - T_\infty} = \left(\frac{1}{\gamma_0(T_w - T_\infty)} \right)$ the

viscosity parameter, $M = \frac{2\sigma B_0^2}{\rho_\infty b(n+1)}$ the magnetic

parameter, $Pr = \frac{\rho C_p \nu}{k}$ the Prandtl number,

$\gamma = \frac{2k_0}{b(n+1)x^{n-1}} (C_w - C_\infty)$ the non-dimensional chemical

reaction parameter, $Gr_t = \frac{g_0 \beta_t (T_w - T_\infty)}{b^2 x^{2n-1}}$ the local

Grashof number, $Gr_c = \frac{g_0 \beta_c (C_w - C_\infty)}{b^2 x^{2n-1}}$ the local modified

Grashof number, $Nr = \frac{kK}{4T_\infty^3 \sigma^*}$ the thermal radiation

parameter, $Ec = \frac{U_w^2}{C_p (T_w - T_\infty)}$ the Eckert number,

$\lambda = \frac{2Q}{b(n+1)\rho_\infty C_p x^{n-1}}$ the heat generation or absorption

parameter, $Sc = \frac{\mu}{\rho_\infty D}$ the Schmidt number and

$\beta = \frac{2n}{n+1}$ the non-linear stretching parameter.

It is worthwhile to mention here that θ_r is negative for liquids and positive for gases. The elimination of γ_0 between the Eq. (1) and the definition of θ_r gives rise

$$\mu = \frac{\mu_\infty}{\left(1 - \frac{\theta}{\theta_r} \right)} \text{ to.}$$

From this relation it is obvious that when $-\theta_r \rightarrow \infty$ then $\mu \rightarrow \mu_\infty$ i.e. the viscosity variation in the boundary layer is negligible. However, the viscosity variation is more significant as $-\theta_r \rightarrow 0$ when $M=0, \beta=1$ and $Gr_t = Gr_c = 0$, the present problem reduces to hydrodynamic boundary layer flow past a stretching sheet whose analytical solutions put forwarded by Crane [2] as follows

$$f(\eta) = 1 - e^{-\eta} \text{ i.e. } f'(\eta) = e^{-\eta} \quad (17)$$

With an aim to test the accuracy of our numerical result for axial velocity $f'(\eta)$, we have compared our result with this analytical solution.

The important characteristics of the present study are the local-skin-friction coefficient C_f and the local Nusselt number N_u defined by

$$\sqrt{Re_x} C_f = - \left(\frac{\theta_r}{1 - \theta_r} \right) \sqrt{\frac{1}{2 - \beta}} f''(0),$$

$$\text{where } C_f = \frac{\tau_w(x)}{\rho U_w^2} \text{ with} \quad (18)$$

$$\tau_w = \mu \left(\frac{\partial u}{\partial y} \right)_{y=0}$$

$$\frac{Nu}{\sqrt{Re_x}} = - \sqrt{\frac{1}{2 - \beta}} \theta'(0),$$

$$\text{where } Nu = \frac{xq_w}{k_\infty (T_w - T_\infty)}, \text{ with} \quad (19)$$

$$q_w = -k_w \left(\frac{\partial T}{\partial y} \right)_{y=0},$$

where $Re_x = \frac{Ux}{\nu}$ is defined as the local Reynolds number.

3. RESULTS AND DISCUSSION

The system of coupled and non-linear ordinary differential Eq. (12) to Eq. (14) along with the boundary conditions Eq. (15) and Eq. (16) have been solved numerically by employing a finite difference scheme. We used Newton's linearization method (Cebeci and Cousteix (1999), Misra and Shit (2009a, 2009b) to linearize the discretized equations. The essential features of this technique are that it is based on a finite difference scheme, which has better stability, simple, accurate and more efficient. Finite difference technique leads to a system which is tridiagonal and therefore speedy convergence as well as economical memory space to store the coefficients. The computational work has been carried out by taking $\delta_\eta = 0.0125$ and further reduction in δ_η does not bring about any significant change. For the purpose of numerical computation it is necessary to assign some valid numerical values to the physical parameters involved in the problem. In this connection, the following data have been used (Naduvanamani and Santosh 2011; Watanabe and Pop 1993, 1995; Afify 2004 and Salem 2007):

$$M \in [0, 6]; \theta_r = -1, -2, -5, -10; \beta = -1, -0.5, 0.5, 1;$$

$$\alpha = 0, \frac{\pi}{6}, \frac{\pi}{4}, \frac{\pi}{3}; Pr = 0.71, 1.5, 7; Nr = 0.5, 1.5, 7;$$

$$\lambda = -0.5, -0.3, 0, 0.5, 1, 2; \gamma = 0.5, 1, 1.5; Sc = 0.5, 1, 1.5$$

The use of non-Newtonian fluid as lubricants is of growing interest for the motion of fluids that contain coarse structures and fibers such as colloidal fluids and liquid crystals. In view of this an attempt has been made to study the micropolar fluids by treating it as lubricants. The quality of lubricating oils and lubricants is attained through purification and manufacturing processes in addition of certain chemical agents. The major consideration in selecting oil for a particular application is viscosity and its variation depends on temperature. However, we used wide range of the values of physical parameters stated above for an illustrative example in order to apply to a greater extend.

Figure 2 shows that our numerical results are in complete agreement with the analytical results of Crane (1970). Figures 3-7 give the variation of axial component of velocity $f'(\eta)$ along with the perpendicular distance η from the sheet for different values of the physical parameters of interest. We observe from Fig. 3 that the axial velocity in the boundary layer region decreases gradually with the increase of the magnetic field strength. This may attribute to the Lorentz force that arises due to the application of an external magnetic field in an electrically conducting fluid. This force has a tendency to slow down the motion of the fluid and thereby decreases momentum boundary layer thickness. It is interesting to note from Fig. 4 that the axial velocity also decreases with the increase of the stretching parameter β .

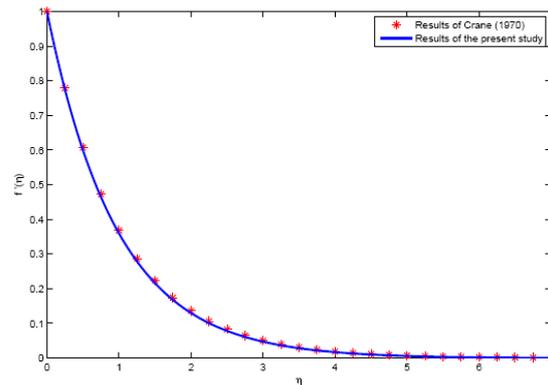


Fig. 2. Comparison of axial velocity with the analytical results of Crane (1970) without applying any external body force

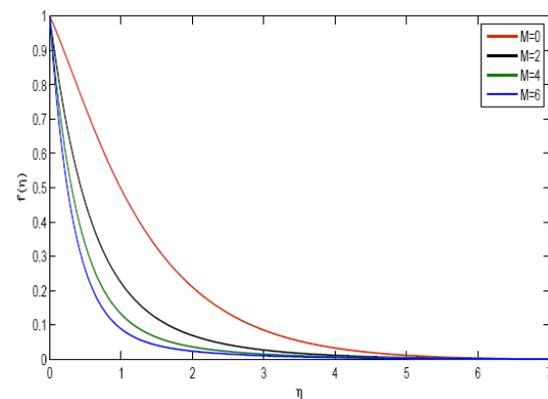


Fig. 3. Variation of $f'(\eta)$ with η for different values of M (with $\theta_r = -2, \beta = -1, \alpha = \pi/4, Pr = 1, Nr = 1, \lambda = 1, \gamma = 0.5$)

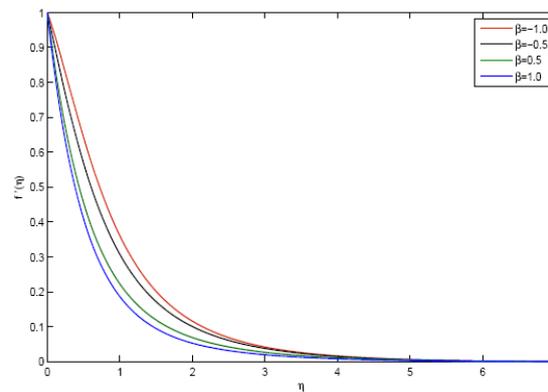


Fig. 4. Variation of $f'(\eta)$ with η for different values of β (with $M = 2, \theta_r = -2, \alpha = \pi/4, Pr = 1, Nr = 1, \lambda = 1, \gamma = 0.5$)

Therefore, non-linearity of the stretching sheet has a reducing effect on the momentum boundary layer thickness. In the present study $\beta = 1$ corresponds to the problem of linear stretching sheet as studied earlier by Shit and Haldar (2011b). Figure 5 depicts the variation of axial velocity for different angle of inclination. It shows that the axial velocity decreases with the increase of the inclination angle α of stretching sheet. It is interesting to note from Fig. 6 that the axial velocity in the boundary layer region decreases with the increasing values of the heat generation/ absorption parameter λ .

However, the viscosity parameter θ_r has increasing effect on the momentum boundary layer thickness as shown in Fig. 7.

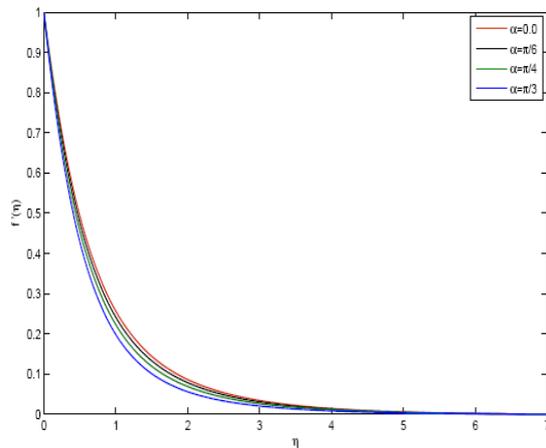


Fig. 5. Variation of $f'(\eta)$ with η for different values of α (with $M = 2, \theta_r = -2, \beta = -1, Pr = 1, Nr = 1, \lambda = 1, \gamma = 0.5$)

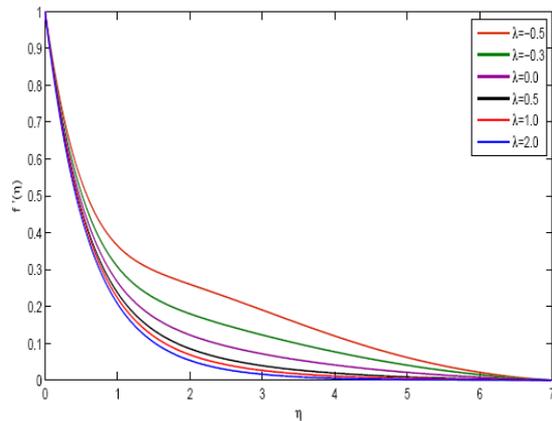


Fig. 6. Variation of $f'(\eta)$ with η for different values of λ (with $M = 2, \theta_r = -2, \beta = -1, \alpha = \pi/4, Pr = 1, Nr = 1, \gamma = 0.5$)

Figures 8-10 illustrate the distribution of dimensionless temperature $\theta(\eta)$ along the height from the stretching sheet for different values of λ, Nr and Pr . We observe from Fig. 8 that the temperature at the sheet gradually decreases with the increase of the heat absorption parameter $\lambda > 0$, whereas, the temperature increases initially up to a certain height above the sheet and beyond which it decreases monotonically for heat generation parameter ($\lambda < 0$). It is also observed that the heat generation/absorption parameter has dual characteristics in the region of thermal boundary layer. Fig. 9 shows that the temperature decreases with the increase of the thermal radiation parameter Nr . It is interesting to note from this figure that the temperature decreases significantly up to a certain value i.e., $Nr = 5$, beyond which no change is observed. The effect of Prandtl Pr on the heat transfer is shown in Fig. 10. It reveals that the temperature is also significantly decreases with the increase of the Prandtl number Pr . The distribution of concentration species for different values of the chemical reaction parameter and the Schmidt number Sc are shown in Fig. 11 and Fig.

12 respectively. The concentration of species in the boundary layer decreases for increasing values of both the parameters γ and Sc . Thus these two parameters are responsible for the reducing of concentration boundary layer thickness.

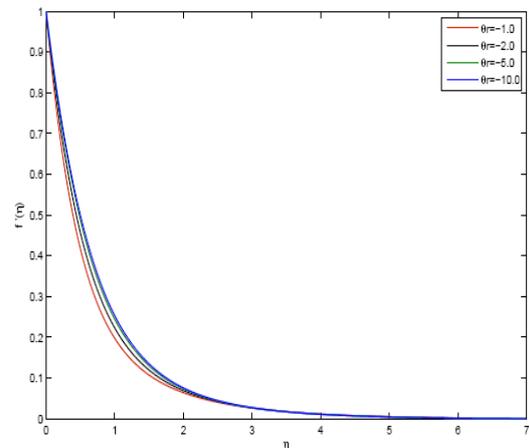


Fig. 7. Variation of $f'(\eta)$ for different values of viscosity parameter θ_r (with $M = 2, \beta = -1, \alpha = \pi/4, Pr = 1, Nr = 1, \lambda = 1, \gamma = 0.5$)

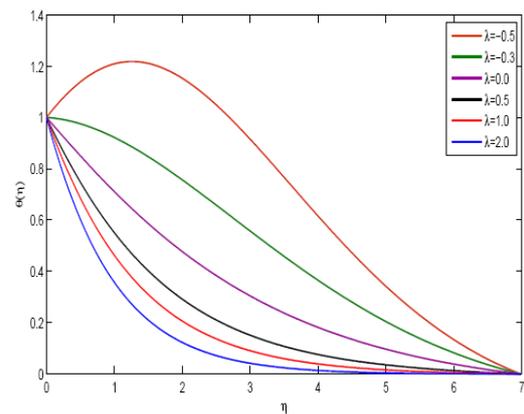


Fig. 8. Distribution of dimensionless temperature $\theta(\eta)$ for different values of λ (with $M = 2, \theta_r = -2, \beta = -1, \alpha = \pi/4, Pr = 1, Nr = 1, \gamma = 0.5$)

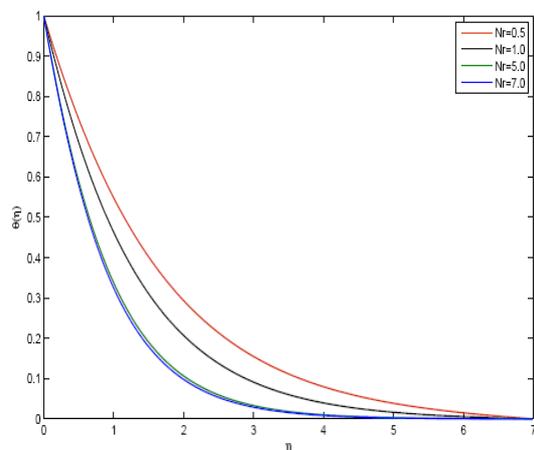


Fig. 9. Distribution of dimensionless temperature $\theta(\eta)$ for different values of thermal radiation parameter Nr (with $M = 2, \theta_r = -2, \beta = -1, \alpha = \pi/4, Pr = 1, \lambda = 1, \gamma = 0.5$)

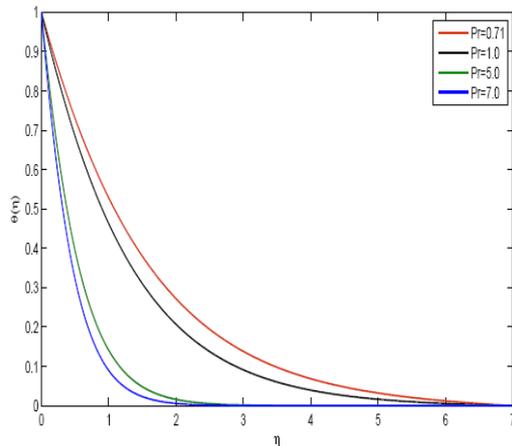


Fig. 10. Distribution of dimensionless temperature $\theta(\eta)$ for different values of Pr (with $M = 2$, $\theta_i = -2$, $\beta = -1$, $\alpha = \pi/4$, $Nr = 1$, $\lambda = 1$, $\gamma = 0.5$)

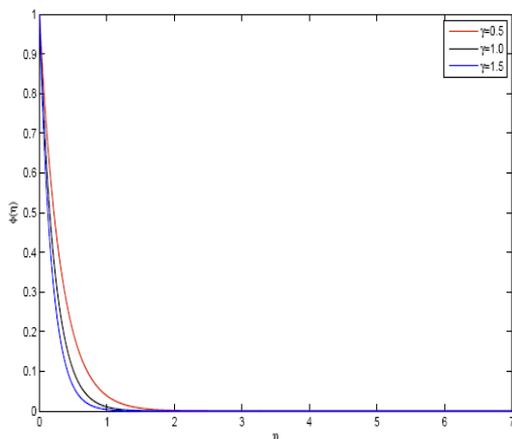


Fig. 11. Concentration profiles for different values of chemical reaction parameter γ (with $M = 2$, $\theta_i = -2$, $\beta = -1$, $\alpha = \pi/4$, $Pr = 1$, $Nr = 1$, $\lambda = 1$)

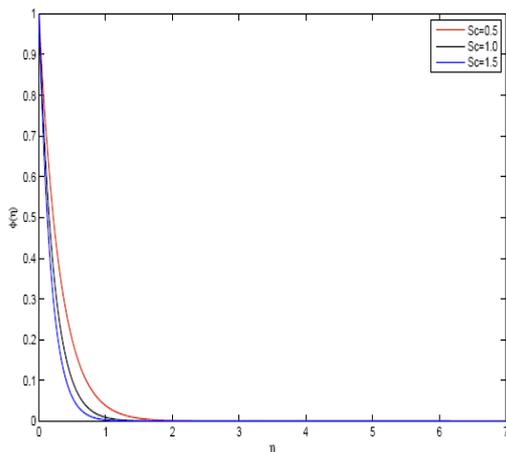


Fig. 12. Concentration profiles for different values of Schmidt number Sc (with $M = 2$, $\theta_i = -2$, $\beta = -1$, $\alpha = \pi/4$, $Pr = 1$, $Nr = 1$, $\lambda = 1$, $\gamma = 0.5$)

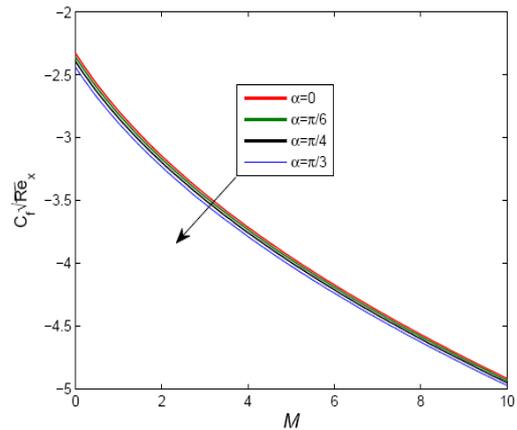


Fig. 13. Variation of skin-friction with the function of M for different values of α (with $\theta_i = -2$, $\beta = -1$, $Pr = 1$, $Nr = 1$, $\lambda = 1$, $\gamma = 0.5$)

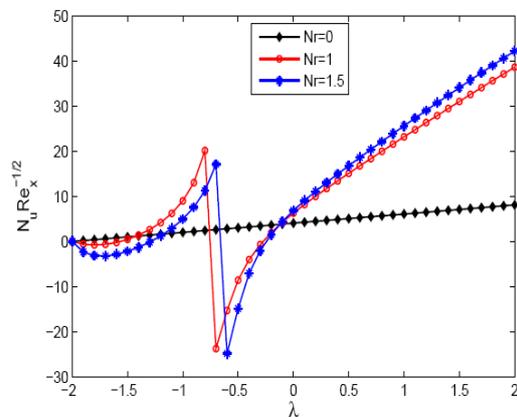


Fig. 14. Variation of Nusselt number with the function of λ for different values of Nr (with $M = 2$, $\theta_i = -2$, $\beta = -1$, $\alpha = \pi/4$, $Pr = 1$)

Figure 13 illustrates the variation of skin-friction $C_f \sqrt{Re_x}$ as the function of Magnetic parameter M for different angle of inclination of the sheet. It reveals that the skin-friction decreases monotonically with increasing magnetic field strength. The skin-friction also decreases with the increase of the inclination angle of the sheet, but the change observed is minimal. For the sake of brevity, it has been observed that the skin-friction coefficient has no change in the absence of thermal radiation. Figure 14 represents the variation of Nusselt number $\frac{Nu_x}{\sqrt{Re_x}}$ that is the rate of heat transfer at

the sheet as a function of heat generation/ absorption parameter λ for different thermal radiation Nr . It is found that the rate of heat transfer gradually increases in the flow opposing region ($\lambda > 0$). However, an anomalous behavior of the Nusselt number is observed in the case of flow assisting region ($\lambda < 0$) in the presence of thermal radiation. It may be pointed out that there exists a critical value (λ_c) of $\lambda < 0$, where a rapid change of the rate of heat transfer takes place. Beyond this critical value of λ , the rate of heat transfer decreases as the heat generation parameter (negative values of λ) increases. It is interesting to note from this figure that the critical value λ_c is different for different

values of the thermal radiation parameter N_r . But, no critical value exists in the absence of thermal radiation.

4. CONCLUDING REMARKS

The effect of thermal radiation and magnetohydrodynamic interaction of flow and heat transfer over an inclined non-linear stretching sheet have been the main concern of this investigation. The temperature dependent variable viscosity has also been the consideration of the present problem. The effect of various key parameters including the angle of inclination (α), magnetic parameter (M), thermal radiation parameter (N_r), heat generation/absorption parameter λ , non-linearity of the stretching sheet (i.e., the parameter β) as well as the chemical reaction parameter γ are examined. The main findings of the present study may be concluded as follows:

- The axial velocity decreases in the boundary layer region for the increasing values of the angle of inclination, magnetic parameter, nonlinearity of the stretching sheet as well as the heat generation or absorption parameter λ .
- The increasing values of the thermal radiation parameter leads to the decreasing of thermal boundary layer thickness. Thus it may be used to increase the rate of cooling of the sheet.
- The interaction of concentration boundary layer decreases with the increase of the chemical reaction parameter γ .
- The skin-friction coefficient decreases with the increase of the magnetic parameter M as well as the angle of inclination of the sheet.

There exists a critical value of λ at which the dual characteristics of the rate of heat transfer is observed in the presence of thermal radiation. Therefore, the effect of thermal radiation plays an important role in controlling heat transfer at the sheet.

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