



# Effect of Oxygen on the Burning Behavior of Liquid and Solid Fuels in a Large-Scale Calorimeter

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## ABSTRACT

The purpose of this experimental study was two-fold: first, to explore and understand the effects of oxygen availability on the combustion of liquid and solid fuels; second, to provide data for comparison with CFD models. Experiments were conducted in the controlled-atmosphere calorimeter of IRSN, called CADUCEE, varying the oxygen concentration in the oxidizing stream and the size of the fire. Polymethylmethacrylate (PMMA) and heptane were used as fuels. Results are found to be in good agreement with the literature data. As the oxygen level decreases, the mass loss rate and flame heat feedback decrease, as well as the flame height and maximum flame temperature, for both fuels whatever the sample size. For heptane pool fires, temperature measurements in the liquid layer reveal a decrease in heat transfer at the fuel surface and inside the fuel with the oxygen molar fraction. For PMMA, the radiative and convective contributions to the total heat flux remain nearly constant, with about 65% and 35% respectively, regardless of sample size and oxygen concentration.

**Keywords:** Fire; Pool fires; Pyrolysis; PMMA; Heptane; Calorimeter.

## NOMENCLATURE

$B$	Spalding mass transfer number	$T$	temperature
$c$	convective	$t$	total
$cp$	condensed phase	$X$	molar fraction
$c_p$	specific heat at constant pressure	$Y$	mass fraction
$D$	pan diameter	$\infty$	ambient
$e$	external	$\beta$	blocking factor
$f$	flame	$\varepsilon$	emissivity
$g$	gas	$\eta$	Nasr model parameter
$h_c$	convective transfer coefficient	$\alpha$	Nasr model parameter
$k$	extinction coefficient	$\sigma$	Stefan-Boltzmann constant
$l$	loss	$\xi$	Tewarson empirical parameter
$L_G$	heat of gasification	$\Delta h$	heat of combustion
$\dot{m}''$	mass loss rate per unit of area	$\chi_r$	flame radiative fraction
$O_2$	oxygen	$\dot{q}''$	heat flux per unit of area
$r$	radiative	$21$	21% oxygen concentration
$r$	stoichiometric oxygen to fuel mass ratio		
$s$	surface		

## 1. INTRODUCTION AND CONTEXT

The effect of oxygen on fuel combustion is of primary importance for fire safety, especially in mechanically-ventilated compartments such as in a nuclear power plant. The amount of oxygen

available for combustion depends mainly on the rate at which replacement air can enter the compartment, due to either natural or forced ventilation. During the fire growth period, when the air supply is not large enough to completely feed the flame, the fire becomes ventilation controlled. A

decrease in the heat feedback from the flame to the fuel surface can be observed, which in turn leads to a decrease in Mass Loss Rate (MLR). This is accompanied by changes in other properties, such as the regression rate of the fuel surface, gas temperature and composition, and heat feedback to the fuel surface.

A model developed by [Utiskul \*et al.\* \(2005\)](#) may be used to express the MLR as a function of the oxygen molar fraction. This model is based on the Quintiere approach ([Quintiere and Rangwala 2004](#)) and some simplifying assumptions. By assuming a small transfer number (called B number, see the definition below) and neglecting the flame radiative effects, [Utiskul \*et al.\* \(2005\)](#) obtained the following relationship:

$$\dot{m}'' = \dot{m}_{21}'' \frac{X_{O_2}}{0.21} + \frac{\dot{q}_{e,r}''}{L_G} \quad (1)$$

More recently, [Nasr \*et al.\* \(2011\)](#) developed a model to determine the fuel MLR in a mechanically-ventilated confined compartment using a global method. This model is based on an energy balance at the fuel surface considering the radiative flux emitted by the flame and non-negligible mass transfer number B

$$\begin{aligned} \dot{m}_f'' L_G = & \frac{h_c \ln(1+B)}{c_p B} \left[ Y_{O_2} \frac{\Delta h}{r} (1 - \chi_r) - c_p (T_s - T_\infty) \right] \\ & + \sigma \varepsilon_f (\alpha Y_{O_2} + \eta)^4 + \sigma (1 - \varepsilon_f) (T_g^4 - T_s^4) - \\ & \sigma (T_s^4 - T_\infty^4) \end{aligned} \quad (2)$$

$$\text{with } B = \left[ Y_{O_2} \frac{\Delta h}{r} - c_p (T_s - T_\infty) \right] / L_G .$$

[Tewarson and Pion \(1976\)](#) determined the MLR of a large variety of solid and liquid fuels from small-scale experiments varying the oxygen concentration. For a wide range of oxygen concentration values, they expressed the MLR as a linear function of the oxygen concentration for all the fuels studied:

$$\dot{m}'' = \frac{\xi}{L_G} X_{O_2} + \frac{\dot{q}_{e,r}'' - \dot{q}_l''}{L_G} \quad (3)$$

Compartment fire experiments were performed by [Peatross and Beyler \(1997\)](#) using either natural or overhead forced ventilation to assess the effect of ventilation on the compartment fire environment. The ventilation rate was varied by changing the vent size in natural ventilation tests and mechanically in forced ventilation tests. Three fuels were used: diesel fuel, wood cribs, and polyurethane slabs. For naturally ventilated fires, it was noted that the vent size and geometry had a significant impact on the vertical temperature and oxygen concentration profiles. Both the temperature and oxygen concentration measurements were representative of two-layer environments. However, in terms of oxygen concentration, forced ventilation fires resulted in a well-mixed compartment

regardless of the ventilation rate. In contrast, temperature measurements showed either a two-layer or linear variation with respect to compartment height, depending on the scenario. The authors showed that reduced oxygen concentrations at the flame base resulted in reduced mass loss rates. The relationship between these burning rates and the oxygen concentration at the flame base was examined, and a correlation was developed. Including data from [Tewarson \*et al.\* \(1981\)](#) and [Santo and Tamanini \(1981\)](#), [Peatross and Beyler \(1997\)](#) found a linear correlation between the MLR and the molar fraction of oxygen

$$\frac{\dot{m}''}{\dot{m}_{21}''} = 10 X_{O_2} - 1.1 \quad (4)$$

This correlation gave a good agreement with experimental results on a small scale, from 0.007 to 0.07 m<sup>2</sup>, and on a larger scale, from 0.3 to 0.55 m<sup>2</sup>, for diesel, heptane and PMMA.

In this context, the present study aims to analyze the effect of oxygen depletion on the combustion of horizontal PMMA slabs and heptane pools. While many studies have been conducted on the combustion of vertically-oriented and tilted slabs of PMMA (e.g. [Pizzo \*et al.\*, 2009](#); [Chen \*et al.\*, 2015](#); [Drysdale and MacMillan 1992](#); [Gollner \*et al.\*, 2013](#)), very few have been on horizontal configurations and even less in under-ventilated conditions. [Rhodes and Quintiere \(1996\)](#) conducted cone calorimeter tests to evaluate the mass loss rate and heat flux at the surface of horizontal black PMMA slabs. [Linteris \*et al.\* \(2005\)](#) have also studied the combustion of black PMMA on a small scale, under cone calorimeter, but for both horizontal and vertical configurations. [Beaulieu and Dembsey \(2008\)](#) conducted bench scale horizontal and single wall vertical orientation experiments for black PMMA, propylene gas and black polyoxymethylene to directly quantify the effects of enhanced ambient oxygen concentration on the flame heat flux. They provided a good explanation of what enhanced ambient oxygen concentration is doing in terms of flame temperature, soot concentration, and thus heat flux. We can also mention the works of [Kacem \*et al.\* \(2016\)](#) who performed free-burning experiments using square PMMA slabs with sides of 10, 20 and 40 cm.

Regarding liquid fuel combustion, many studies have been conducted on the subject in recent decades, owing to its high heat of combustion. A lot of experimental studies have been carried out, varying the pool size, the lip, size and material of the pan, the initial fuel layer, the initial fuel temperature, to name but a few examples. They showed a larger scatter in the reported data, especially those concerning the pyrolysis rate. Following [Zabetakis and Burgess \(1961\)](#) the following relationship can be used to represent the burning rate per unit area as a function of pool diameter, D:

$$\dot{m}'' = \dot{m}_{\max}'' \left[ 1 - \exp(-k \beta D) \right] \quad (5)$$

where  $k$  is the extinction coefficient and  $\beta$  the mean-beam length correction. The maximum burning rate per unit area,  $\dot{m}''_{max}$ , is also referred to in the literature by Babrauskas (1983) as  $\dot{m}''_{D\infty}$ , the mass burning rate for an infinite diameter pool. Average values of  $\dot{m}''_{D\infty}$  and  $k\beta$  for steady burning of more than 20 liquids and one solid (PMMA) are given in Babrauskas (1983). For heptane,  $\dot{m}''_{D\infty} = 0.101 \text{ kg}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$  and  $k\beta = 1.1 \text{ m}^{-1}$ , based on the experiments of Kung and Stavrianidis (1982) and Tarifa (1967). It is worth noting that Eq. (5) is valid for  $D > 0.2 \text{ m}$ , where heat transfer is dominated by radiation. As mentioned previously, Tewarson *et al.* (1981) experimentally studied the effect of oxygen on the pyrolysis rate. Their tests included heptane pool fires with a diameter of 0.1 m and oxygen concentrations ranging from 27.3 to 15.7%.

The objective of this study is twofold: to better understand the effects of an oxygen-depleted atmosphere on the combustion of solid and liquid materials and to provide data needed to validate the numerical simulation tools of a fire. For this purpose, the calorimeter CADUCEE (Controlled Atmosphere Device for Unburnt and Carbon Emission Evaluation) was used. This calorimeter, designed and developed by IRSN (Institut de Radioprotection et de Sûreté Nucléaire), makes it possible to conduct experiments on solid, liquid or gaseous fuels at small and medium scales. This article is organized as follows: the experimental device is presented, as well as the associated metrology, the ignition procedure of the fuel is then detailed, the results obtained concerning the influence of ambient oxygen concentration on the combustion of horizontal PMMA slabs and heptane pools are finally analyzed and compared with those of the literature.

## 2. DESCRIPTION OF EXPERIMENTS

The experiments were conducted using the CADUCEE apparatus shown in Fig. 1. It is composed of a combustion chamber of  $22 \text{ m}^3$ , with a height of 3.1 m and a diameter of 2.9 m. This calorimeter has been developed by IRSN to simulate the depleted oxygen environments of a fully-developed fire, and even the fuel-rich post-flashover fire environment. This was achieved using a nitrogen dilution of the incoming gases and a suitable flow rate through the combustion chamber. The air/nitrogen mixture is injected from the bottom of the combustion chamber (Fig. 1). The oxygen level of the oxidizing mixture is measured and controlled at three different positions in the combustion chamber. The upper part of the calorimeter is composed of an exhaust system, which recovers the combustion products before analyzing them in the test section. More details (metrology, estimation of measurement uncertainties) about the CADUCEE device can be found in Coutin *et al.* (2016).

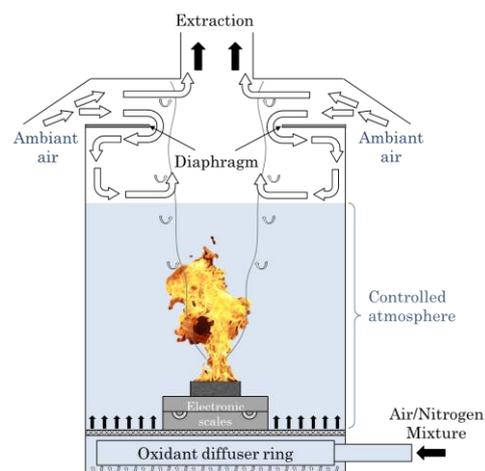
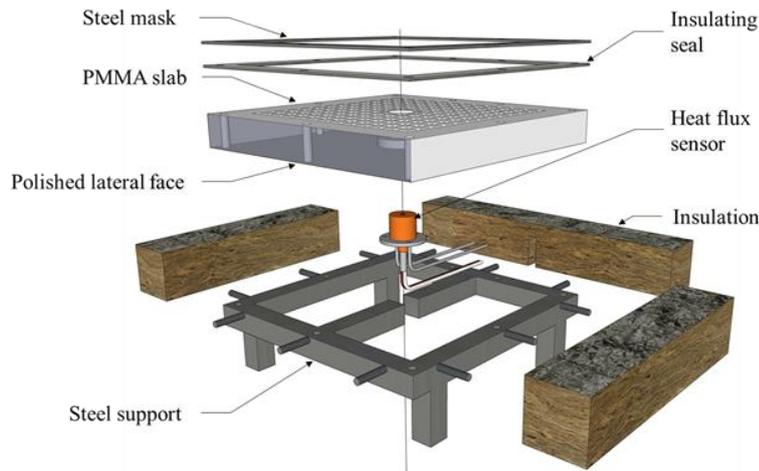


Fig. 1. View (top) and schematic diagram (bottom) of the CADUCEE calorimeter of IRSN.

Two fuels were chosen here: one is solid, the PMMA, the other liquid, heptane of technical quality. PMMA is often used to containment windows for glove boxes containing radioactive components in nuclear facilities. This “well-behaved” polymer doesn’t intumesce or produce char residues, and its thermo-physical properties are relatively well known. Heptane was chosen as liquid fuel, due to its high heat of combustion.

Solid fuel experiments were conducted on square slabs of PMMA with areas of 0.04, 0.16 and  $0.36 \text{ m}^2$  and thickness of 30 mm. PMMA slabs were mounted horizontally on a steel support to avoid thermal deformations and covered with a steel screen to delimit the burning area (Fig. 2). One of the four lateral faces was initially polished to allow observation of the transient evolution of the PMMA regressing surface. The others were insulated with 50-mm-thick low emissivity foil-faced glass mineral wool batts to avoid any inopportune lateral ignition. To measure the total or radiative heat fluxes at the burning surface, a total heat flux sensor Medtherm 64-2-20T or an ellipsoidal radiometer Medtherm 64EP-2-21495T was embedded in a hole predrilled at the center of the slab. The gage face



**Fig. 2. Experimental setup for PMMA experiments.**

was placed flush with the sample surface. This technique was also used by Rhodes and Quintiere (1996), Beaulieu and Dembsey (2008) and Pizzo *et al.* (2015). Both sensors were cooled with water at ambient temperature during the tests and a very low nitrogen flow (about 2 L.min<sup>-1</sup>) was used to avoid the entrance of soot particles into the ellipsoidal radiometer cavity.

Each experiment was performed twice, one to measure the radiative heat flux and one to measure the total heat flux. The experimental apparatus, including the support and the slab, was located on a Sartorius precision scale ( $\pm 0.1$  g) to measure the time evolution of the sample mass. Gas temperatures were measured with an array of eleven K-type thermocouples of 1 mm diameter located, before ignition, at 0.05, 0.1, 0.15, 0.2, 0.3, 0.4, 0.5, 1.0, 1.5, 2.0, and 2.5 m from the upper face of the slab. The oxidizing flow rate was set to 1500 m<sup>3</sup>.h<sup>-1</sup> for slabs with areas of 0.04 and 0.16 m<sup>2</sup>, and to 2500 m<sup>3</sup>.h<sup>-1</sup> for 0.36-m<sup>2</sup> slabs. Smoke was exhausted at a rate of 2500, 4000, or 7000 m<sup>3</sup>.h<sup>-1</sup> for slabs with areas of 0.04, 0.16 and 0.36 m<sup>2</sup>, respectively. The initial fuel temperature was about 20°C.

One of the major experimental challenges is to provide a homogeneous ignition of the solid upper face in the CADUCEE facility. The held solution consisted in grooving the upper surface of the slab and filling the 2-mm-deep grooves with a small amount of ethanol. A 21.0% oxygen concentration was kept during the ignition phase for a period depending on the slab size (i.e. 500, 900 and 1000 s for the slabs with areas of 0.04, 0.16 and 0.36 m<sup>2</sup>, respectively), ensuring that the ethanol was totally consumed (about 120 s), the grooves had totally disappeared, the burning surface was plane, and the flame covered the whole surface. After that, the oxidizing mixture was injected into the combustion chamber at the desired level of oxygen. The extinction is provided by suddenly increasing the proportion of nitrogen into the oxidant flow to lower the oxygen concentration below 10.0%. Qualification tests have highlighted a limiting oxygen concentration below which the flame

extinction occurs. This concentration is about 17.5% for the PMMA regardless of the sample size.

This value is close to the literature values from different scale experiments (ISO 4589, (1996), Ebdon *et al.*, 2000a and 2000b; Laachachi *et al.*, 2005; Yang and Nelson, 2006, Zhubanov and Gibov, 1988; Price *et al.*, 2002).

Heptane fuel was burned in two borosilicate glass containers (Table 1). The time evolution of the liquid fuel mass was measured using a Sartorius precision scales ( $\pm 0.01$  g). Twelve K-type thermocouples of 1 mm diameter are positioned along the flame axis at 0.05, 0.1, 0.15, 0.2, 0.25, 0.35, 0.45, 0.55, 1.05, 1.55, 2.05, and 2.55 m from the initial level of the liquid pool. For the largest pan, one thermocouple is added at 0.01 m from the pan bottom in order to measure the time evolution of the fuel temperature. The inlet oxidizing flow and exhaust flow rates were set to 1500 m<sup>3</sup>.h<sup>-1</sup> and 2500 m<sup>3</sup>.h<sup>-1</sup> respectively, and the initial fuel temperature was about 20°C.

Ignition was provided with a propane burner. The 21% oxygen concentration was kept during 180 s ensuring a stable combustion. Qualification tests have shown a limiting oxygen concentration about 14.5% closed to the literature values (Loo *et al.*, 2013; Fourneau, 2013).

**Table 1 Fuel pan dimensions and initial liquid fuel height**

Internal diameter, mm	Pan		Fuel height, mm
	Thickness, mm	Height, mm	
196	3	20	17
116	2	14	12

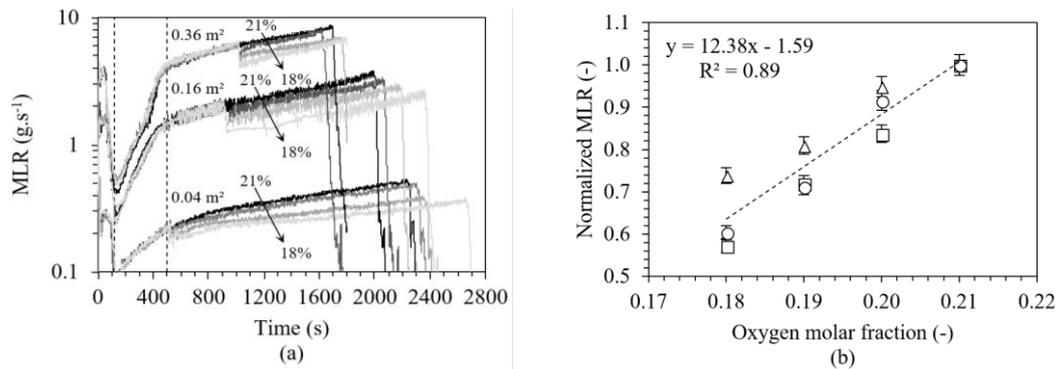
### 3. RESULTS AND DISCUSSION

#### 3.1. Solid Fuel

Table 2 summarizes PMMA burning results, along with the time periods for averaging.

**Table 2 PMMA experiment summary.**  $t_{inj}$  corresponds to the instant at which the oxidizing mixture was injected at the desired oxygen level

Surface area ( $m^2$ )	$X_{O_2}$	$t_{inj}(s)$	Averaging period (s)	$\dot{m}(g.s^{-1})$ $\pm 3\%$	$\dot{q}_t''(kW.m^{-2})$ $\pm 4\%$	$\dot{q}_r''(kW.m^{-2})$ $\pm 4\%$	$\dot{q}_e''(kW.m^{-2})$ $\pm 4\%$
0.04	0.21	-	2000-2200	0.491	40.9	25.9	15.0
	0.20	500	2000-2200	0.450	36.9	23.7	13.2
	0.19	500	2000-2200	0.350	28.7	19.1	9.6
	0.18	500	2000-2200	0.297	24.4	15.9	8.5
0.16	0.21	-	1800-2000	3.395	59.5	39.1	20.4
	0.20	900	1800-2000	2.842	52.7	36.8	15.9
	0.19	900	1800-2000	2.445	47.9	29.8	18.2
	0.18	900	1800-2000	1.943	42.9	28.5	14.4
0.36	0.21	-	1200-1600	7.273	-	-	-
	0.20	1000	1200-1600	6.898	-	-	-
	0.19	1000	1200-1600	5.887	-	-	-
	0.18	1000	1200-1600	5.370	-	-	-



**Fig. 3. (a) Time evolution of the MLR and (b) normalized MLR vs. oxygen molar fraction (○ 0.04  $m^2$ , □ 0.16  $m^2$ , △ 0.36  $m^2$ ).**

### 3.1.1. Mass Loss Rate

The MLR is calculated by deriving the time evolution of the sample mass and applying a 30-s moving centered average. Figure 3(a) shows the time evolution of the MLR for the three sample sizes and the four oxygen concentrations studied. Four periods can be observed: the first, from 0 to 120 s, corresponds to ethanol combustion; the second, from 120 to 500 s, to the time required for the flame to cover the upper face of the slab, which agrees with values obtained by Pizzo *et al.* (2015); and the third, from 500 s, to PMMA burning until extinction.

During this period, an increase of the MLR can be observed. The bursting of bubbles leads to the formation of cavities that increases the specific area of the burning surface, which in turn leads to an increase of the total MLR and heat flux at the slab surface. Moreover, increasing the heat flux tends to increase the number of bubbles while reducing their size, contributing further to a rise in specific area (Kashiwagi and Ohlemiller, 1982; Marquis *et al.*, 2014; Beaulieu, 2005). The fourth period corresponds to the extinction of the slab provided by an increase of nitrogen in the oxidizing mixture, leading to an oxygen concentration less than 10%. As shown in Fig. 3(a), the higher the sample size, the higher the heat release rate and the heat feedback to the fuel surface, and thus the higher the

MLR. An average value of the MLR can be calculated over a period depending on the sample size (Table 2). This period corresponds to that when the MLR shows a nearly constant rate of change. The averaged mass loss rate values are then normalized with that obtained over the same period for an oxygen concentration of 21%. As shown in Fig. 3(b), a linear correlation can be found between the normalized MLR per unit area and the oxygen molar fraction independently of the sample size as

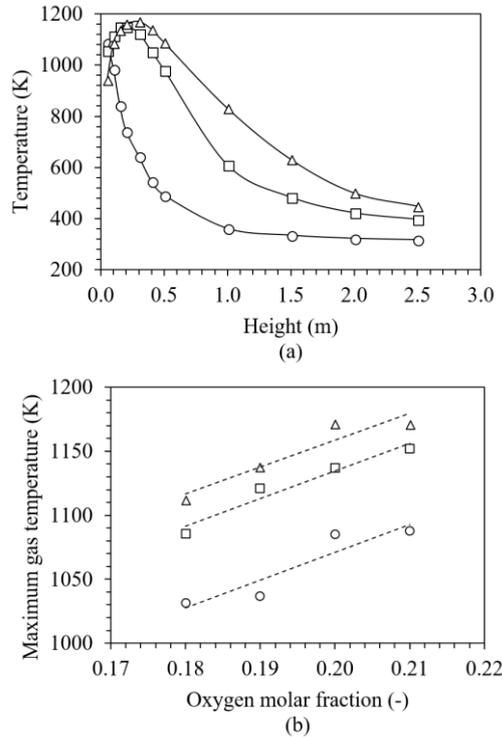
$$\frac{\dot{m}''}{\dot{m}''_{21}} = 12.4X_{O_2} - 1.6 \quad (6)$$

### 3.1.2. Gaz Temperature

Figure 4(a) shows the time-averaged gas temperature versus the height measured from the initial fuel surface for the three sample sizes and a 21% ambient oxygen concentration. The three flame regions observed by McCaffrey (1979) are clearly identified. For example, for the smallest sample size, the persistent flame region is located between 0 and 0.2 m and the plume region above 1.1 m, the intermittent flame region being located between the two. We can observe in Fig. 4(a) that the maximum value of the gas temperature and the height at which this maximum is obtained increase with the sample size. In addition, the larger the sample size, the slower the decrease in temperature. The maximum gas temperature is between 1080 and

1180 K, in agreement with those obtained by Kacem *et al.* (2016) (~1190 K) for 0.01 m<sup>2</sup> slabs and by Beaulieu and Dembsey (2008) (1184 ± 100 K) for 0.011 m<sup>2</sup> slabs.

As expected, reducing the oxygen level leads to a decrease in maximum gas temperature for all sample sizes (Fig. 4(b)), as also observed by Santo and Tamanini (1981).



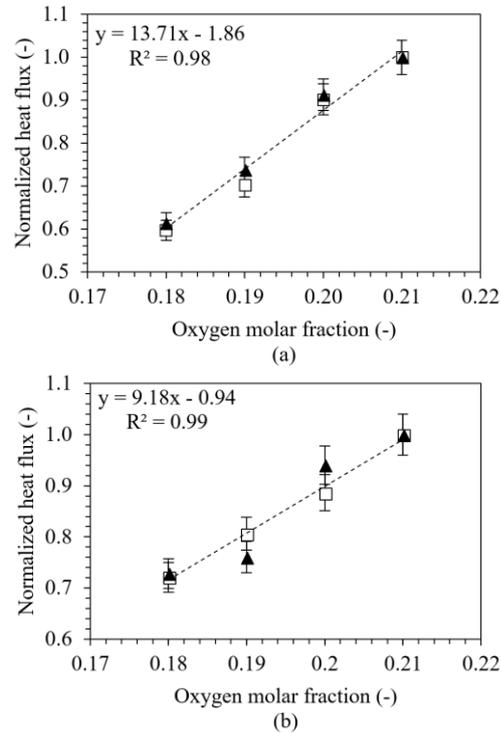
**Fig. 4. (a) Gaz temperature vs. height for the 21% ambient oxygen concentration and (b) maximum gas temperature vs. oxygen molar fraction (○ 0.04 m<sup>2</sup>, □ 0.16 m<sup>2</sup>, △ 0.36 m<sup>2</sup>).**

### 3.1.3. Heat Flux

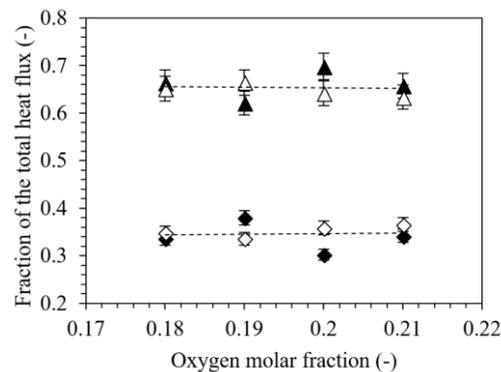
As mentioned above, total and radiative heat fluxes were measured at the center of the slab using a total heat flux sensor and an ellipsoidal radiometer. The convective heat flux was calculated as the difference between the total heat flux and the radiative heat flux. Table 2 gives the averaged values of heat fluxes versus the oxygen concentration for the slabs with areas of 0.04 and 0.16 m<sup>2</sup>. Measurements were not possible for larger slabs due to problems of condensation of MMA and/or liquid PMMA projections on the sensitive surface of the sensors.

It is obvious that the total heat flux increases with the sample size and oxygen concentration. For all experiments, radiation dominates. Normalized by the values obtained for the 21% ambient oxygen concentration, the total and radiative heat fluxes are plotted as a function of the oxygen concentration in Fig. 5. As observed for the MLR, a linear decrease of the normalized heat fluxes with the oxygen molar fraction can be observed. What is more surprising is that the contribution of radiation to the total heat

flux remains almost constant, with approximately 65%, leading to a convective contribution of about 35% (Fig. 6).



**Fig. 5. Normalized heat fluxes versus oxygen molar fraction for samples of (a) 0.04 m<sup>2</sup> and (b) 0.16 m<sup>2</sup> (□ Total, ▲ Radiative).**



**Fig. 6. Radiative and convective contributions to the total heat flux versus oxygen molar fraction for samples of 0.04 m<sup>2</sup> (▲ Radiative fraction, ◆ Convective fraction) and 0.16 m<sup>2</sup> (△ Radiative fraction, ◇ Convective fraction).**

## 3.2. Liquid fuel

Table 3 summarizes heptane burning results, along with the time periods for averaging.

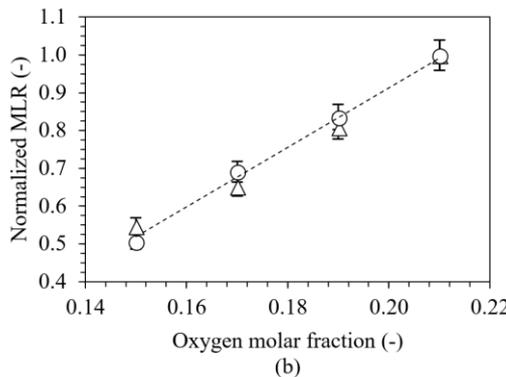
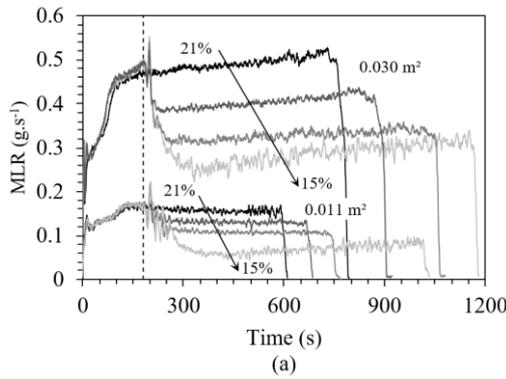
### 3.2.1. Pyrolysis Mass Loss Rate

Figure 7(a) shows the time evolution of the MLR for the 0.011-m<sup>2</sup> and 0.03-m<sup>2</sup> heptane pools and ambient oxygen concentrations ranging from 15 to 21%. From 0 to 180 s, fire develops in a 21% ambient oxygen concentration. Subsequently, a

quasi-steady burning period is observed before flame extinction due to fuel depletion. As done previously, a more general approach may be used by averaging the MLR over the steady-burning period (Table 3) and normalizing the time-averaged value with the MLR that results from burning in normal oxygen concentrations (Fig. 7 (b)).

**Table 3 Heptane experiment summary.  $t_{inj}$  corresponds to the instant at which the oxidizing mixture was injected at the desired oxygen level.**

Pool area ( $m^2$ )	$X_{O_2}$	$t_{inj}$ (s)	Averaging period (s)	$\dot{m}$ ( $g.s^{-1}$ ) $\pm 3\%$
0.011	0.21	-	300-590	0.156
	0.19	180	300-590	0.130
	0.17	180	300-590	0.108
	0.15	180	800-1000	0.079
0.030	0.21	-	300-730	0.495
	0.19	180	300-730	0.401
	0.17	180	300-730	0.323
	0.15	180	300-730	0.271



**Fig. 7. (a) Time evolution of MLR and (b) normalized MLR versus oxygen molar fraction ( $\circ$  0.011  $m^2$ ,  $\Delta$  0.030  $m^2$ ).**

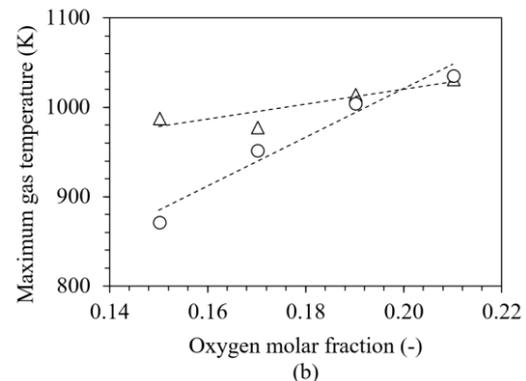
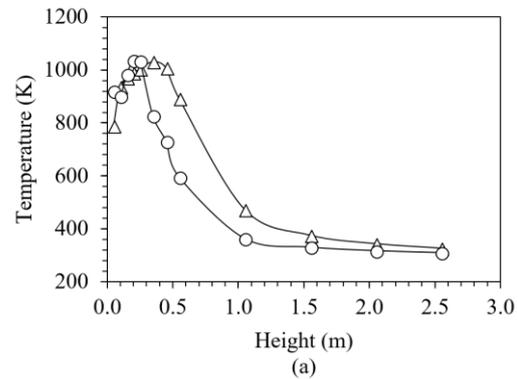
Although there is little data, a linear decrease of the normalized MLR with the oxygen concentration can be observed

$$\frac{\dot{m}''}{\dot{m}''_{21}} = 7.9X_{O_2} - 0.7 \quad (7)$$

### 3.2.2. Gas Temperatures

Figure 8(a) shows the evolution of the time-averaged raw gas temperature (without radiation

correction) with height (measured from the initial pool level) in a 21% oxygen concentration for heptane pools with areas of 0.011 and 0.030  $m^2$ . The three flame regions observed by McCaffrey (1979) are clearly identified and the maximum flame temperatures are nearly the same, around 1030 K, which can be favorably compared with that obtained by Chen *et al.* (2012) for a 0.031- $m^2$  heptane pool fire, with 973 K. As shown in Fig. 8(b), the maximum gas temperature increases with the oxygen concentration, and this effect is more pronounced for the smaller pool size. It can be clearly seen from Fig. 9 that the visible flame height increases with the pool size and oxygen concentration, because of an increase in MLR (Fig. 7(a)).



**Fig. 8. (a) Gaz temperature vs. height in a 21% oxygen concentration and (b) maximum gas temperature vs. oxygen molar fraction ( $\circ$  0.011  $m^2$ ,  $\Delta$  0.030  $m^2$ ).**

### 3.2.3. Fuel Temperature

Figure 10 shows the time evolution of the liquid temperature at 1 cm from the container bottom for the 0.030- $m^2$  heptane pool fire and for the four oxygen molar fractions considered. It is important to note that no boiling has been observed. In a 21% oxygen concentration, an increase of the fuel temperature can be observed up to a value close to the boiling temperature (371.3 K) when the burning surface is just above the thermocouple. When the interface reaches the thermocouple location, a slight decrease followed by a plateau is observed. Subsequently, the thermocouple is in the hot gas layer just above the interface, which explains the

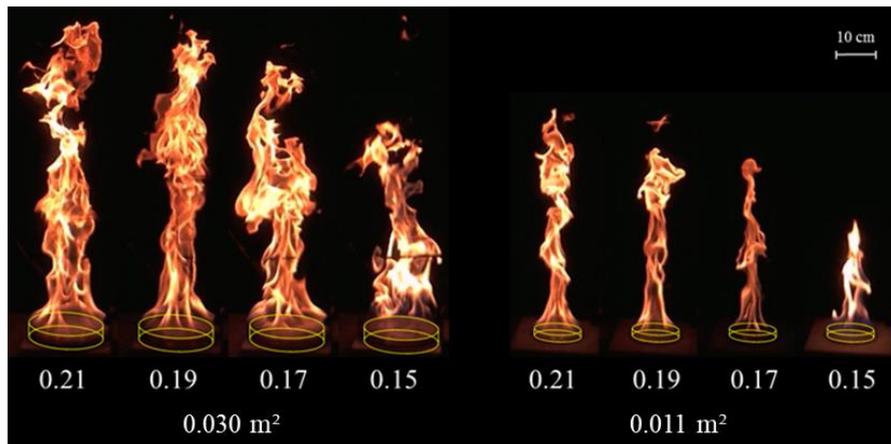


Fig. 9. Snapshots of 0.030 and 0.011 m<sup>2</sup> heptane pool fires for oxygen concentrations in the range of 15-21%.

sharp increase in temperature, up to 415-425 K. This is followed by a slight increase when the flame gets closer to the flame. Finally, a second sharp increase is observed when the thermocouple is in the flame region. Current results are comparable to those found by Chen *et al.* (2012), namely 371.8 K for the boiling temperature and 403-418 K for the hot gases.

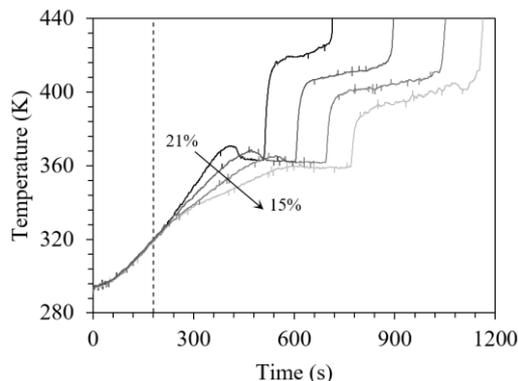


Fig. 10. Time evolution of the liquid temperature at 1 cm from the container bottom for the 0.030-m<sup>2</sup> heptane pool fire and oxygen concentration in the range of 15-21%.

As the oxygen molar fraction decreases, the same trend is observed, but with lower temperature levels. For example, the plateau temperature decreases by about 10 K as the ambient oxygen concentration is decreased from 21 to 15%. This general comportment can be explained by a decrease of the heat transfers at the fuel surface and inside the fuel. Further work is required to assess this statement.

#### 4. COMPARISON WITH LITERATURE RESULTS

Figure 11 shows some literature results on the MLR of liquid fuels as a function of the pan diameter at 21% ambient oxygen concentration. A large scatter is observed that can be attributed to several factors, such as the geometry of the container, the nature of the material that constitutes it (e.g. steel, stainless

steel or borosilicate glass) the quality of heptane (technical or pure) (Loo *et al.*, (2016), the environmental conditions (e.g. ambient temperature or ventilation) or the lip height. Despite this, the results obtained in the present study are in good agreement with those of literature.

Regarding the effect of oxygen on the burning rate, Fig. 12 gives a comparison of the current results with the literature data. Included are data from experiments with different fuel types and fuel sizes. The use of normalized MLR allows relevant comparison. Good agreement is generally found, as well as with the empirical correlation of Peatross and Beyler (see Eq. (4)). One of the reasons for this good concordance may be that this correlation was obtained in conditions for which external heat fluxes were negligible, as is the case for small and moderate fire experiments in CADUCEE (i.e. heat release rate typically less than 250 kW).

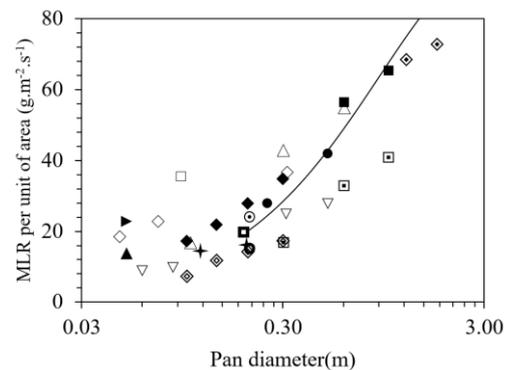
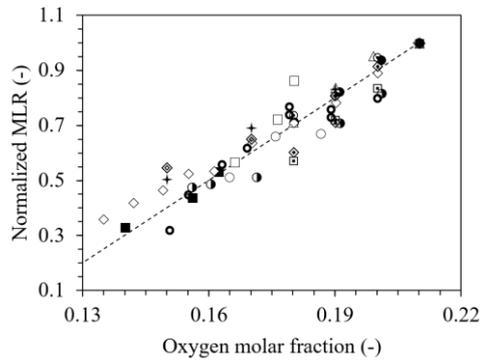


Fig. 11. MLR per unit of area versus pan diameter in 21% ambient oxygen concentration.

Symbols: □ Tawarson *et al.* (1981), — Babrauskas correlation (1983), ◇ Kung and Stavrianidis (1982), ● Tarifa (1967), ○ Chen *et al.* (2012), ⊙ Chen *et al.* (2012), ■ Loo *et al.* (2016), ▲ Hayasaka (1997), ► Hayasaka (1997), ▽ Mulholland *et al.* (1989), □ Koseki and Yumoto (1988), ◇ Gore *et al.* (1991), △ Buch *et al.* (1997), ■ Klassen and Gore (1994), ◇ Kang *et al.* (2010), ◆ Kang *et al.* (2010), + CADUCEE (present study).



**Fig. 12. Normalized MLR versus oxygen molar fraction. Comparison between current results:  $\blacktriangle$  Heptane – 0.011 m<sup>2</sup>,  $\blacklozenge$  Heptane – 0.030 m<sup>2</sup>,  $\blacklozenge$  PMMA – 0.04 m<sup>2</sup>,  $\blacksquare$  PMMA – 0.16 m<sup>2</sup>,  $\odot$  PMMA – 0.36 m<sup>2</sup>. Comparison with literature result:  $\square$  Peatross and Beyler (1997) – Diesel – 0.3 m<sup>2</sup>,  $\blacksquare$  Peatross and Beyler (1997) – Diesel – 0.5 m<sup>2</sup>, --- Peatross and Beyler correlation (1997) – Eq. (4),  $\circ$  Tewarson *et al.* (1981) – PMMA – 0.073 m<sup>2</sup>,  $\bullet$  Tewarson *et al.* (1981) – PMMA – 0.068 m<sup>2</sup>,  $\bullet$  Tewarson *et al.* (1981) – Heptane – 0.0068 m<sup>2</sup>,  $\triangle$  Santo and Tamanini (1981) – PMMA – 0.07 m<sup>2</sup>,  $\bullet$  Coutin *et al.* (2016) – Heptane – 0.07 m<sup>2</sup>,  $\blacklozenge$  Brohez *et al.* (2008) – Pyridine – 0.0061 m<sup>2</sup>.**

## 5. CONCLUSION

The controlled-atmosphere calorimeter CADUCEE of IRSN was used to study the effect of ambient oxygen concentration on the burning behavior of solid (PMMA) and liquid (heptane) fuels. Square slabs of clear PMMA with areas of 0.04, 0.16 and 0.36 m<sup>2</sup> and heptane pools with areas of 0.011 and 0.030 m<sup>2</sup> were used. Oxygen concentration varied from 18 to 21% for PMMA, and from 15 to 21% for heptane. From the results, some conclusions can be drawn:

- Current data on time-averaged normalized MLR, heat flux, and flame temperature are in good agreement with those reported in the literature.
- The normalized MLR linearly decreases with the oxygen concentration, with a slope of 12.4 for PMMA and 7.9 for heptane, compared to a slope of 10.0 for the Peatross and Beyler correlation.
- Reducing the oxygen level leads to a decrease in the flame height and of the maximum flame temperature for both fuels, whatever the sample size;
- For heptane pool fires, temperature measurements in the liquid layer reveal a decrease in heat transfers at the fuel surface and inside the fuel with the oxygen molar fraction.
- Although the total and radiative heat fluxes measured at the center of the PMMA slabs decrease with the oxygen concentration, the radiative and

convective contributions to the total heat flux remain almost constant, with about 65% and 35% respectively, regardless of sample size and oxygen concentration.

In the continuity of this study, further work is in progress first, to collect additional data on heptane pool fires; second, to evaluate the flame heat feedback to the burning surface of liquid pools, using borosilicate glass pans that are specifically designed to insert a heat flux sensor at the center of the pool.

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